

**Hydrogen, Fuel Cells & Infrastructure Technologies Program**

**2005 Annual Review**

Washington, DC, May 23-27, 2005

## **Non-Precious Metal Catalysts**

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Christine Hamon, Barbara Piela, John Ramsey, Francisco Uribe**

*and*

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***This presentation does not contain any proprietary or confidential information***

## Project Objective & Focus

### Objective:

*Develop low-cost non-precious metal oxygen reduction reaction (ORR) catalyst for the polymer electrolyte fuel cell (PEFC) cathode with similar activity and performance durability to the currently used noble-metal based cathode catalysts.*

### Focus:

- *Transition metal macrocycles (e.g. pyrolyzed TPP & TMPP chelates of Co & Co/Fe) – advanced phase; progress to date summarized in this presentation*
- *Metal chalcogenides (e.g. Ru-based and Ru-free catalysts) – early phase, very promising initial results*
- *Metal oxides (e.g. NiO, Co<sub>2</sub>O<sub>3</sub>, NiCoO<sub>2</sub>, perovskitic LaSrCo oxides, CuMn oxides) – part of future research*

## Funding & Milestones

### Funding:

*FY 2004 (started January 29, 2004)*

**\$118K**

*FY 2005*

**\$350K**

*Project reviewed for the first time*

### 2004 & 2005 Milestones:

- *Develop techniques for electrochemical characterization of non-precious metal catalysts under conditions relevant to fuel cell operation. – June 2004*
- *Perform initial electrochemical/pH stability experiments on pyrolyzed macrocycle transition metal (PMTM) catalysts. – March 2005*
- *Identify active reaction site(s) for oxygen reduction on pyrolyzed  $N_4$ -chelate electrocatalyst in polymer electrolyte fuel cell. – September 2005*

## Selected Collaborations & Interactions (©)

- **Transition Metal Macrocycles**

*University of New Mexico, Professor Plamen Atanassov – synthesis and supply to LANL of Co, Co/Fe porphyrin catalysts for the presented research; half-cell performance screening; TEM catalyst characterization; more*

- **Metal Chalcogenide Catalysts**

*Université de Poitiers, Professor Nicolas Alonso-Vante – synthesis, initial electrochemical & non-electrochemical characterization of chalcogenide catalysts*

*University of Illinois, Professor Andrzej Wieckowski – alternative method of catalyst synthesis, half-cell performance screening*

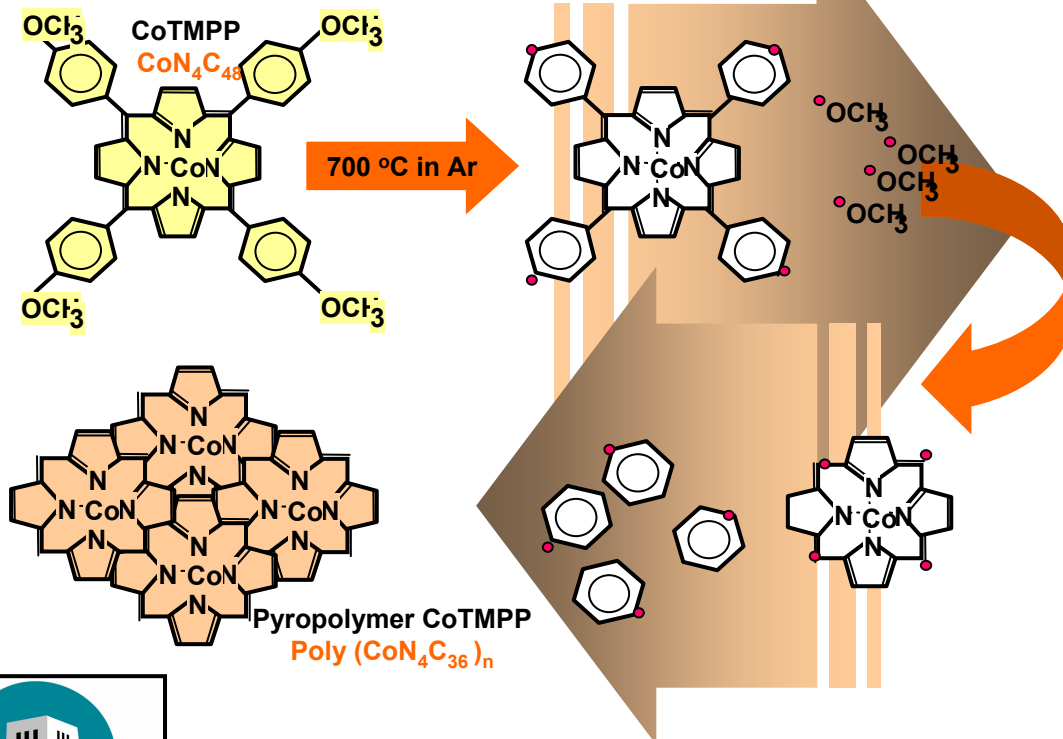
- **Non-Precious Metal Catalysts for Portable Systems**

*Mesoscopic Devices, Inc., Valerie Hovland – catalysts, membranes, MEAs, and feed schemes for mixed-reactant fuel cells*

- **Activated Polyoxometalates**

*OSRAM SYLVANIA, Joel Christian – PEFC activity evaluation by LANL*

# Pyrolysis of Metal Porphyrins A Major Chemical Transformation



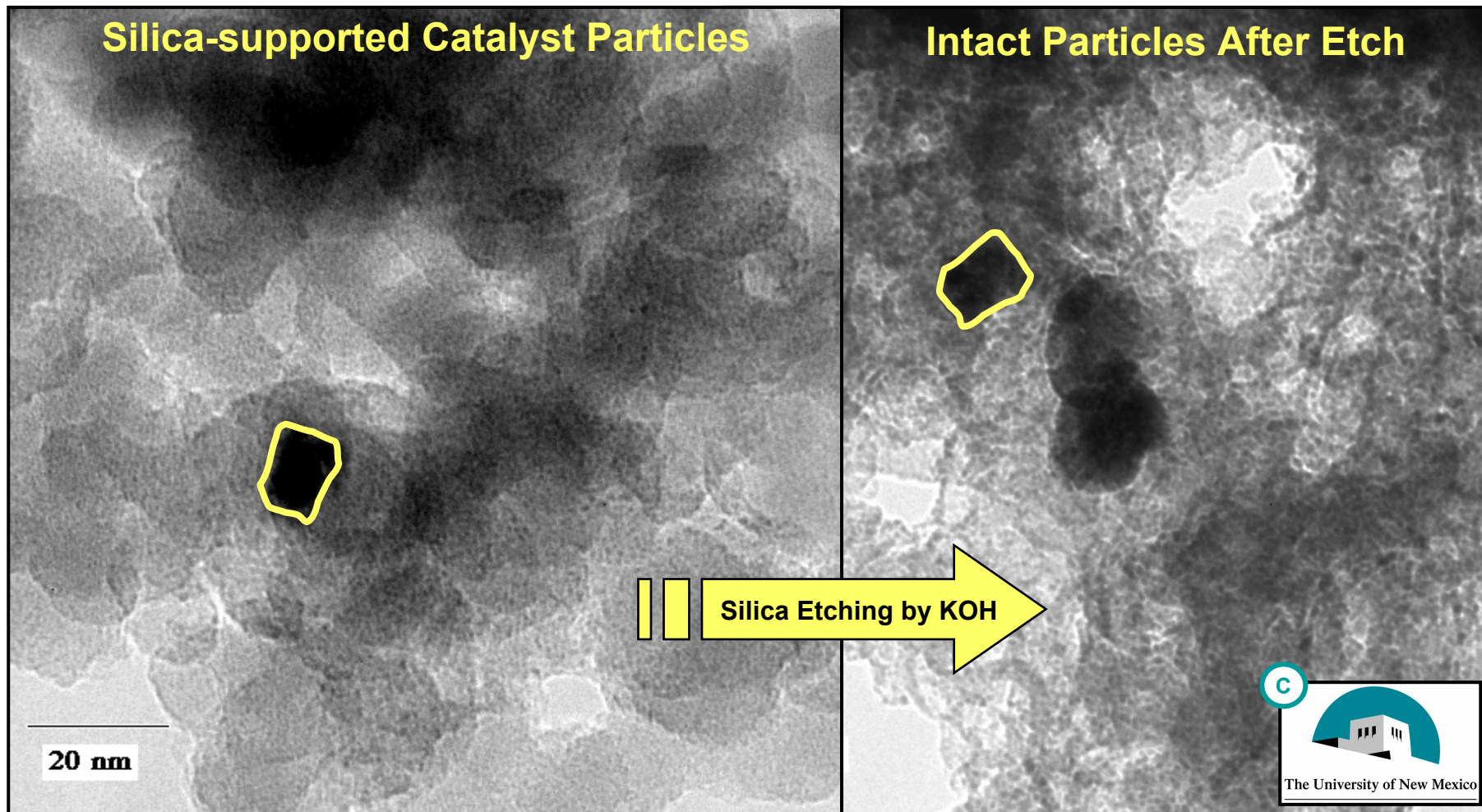
- (1) Heat treatment:  
18 min - 5 hours: 300°C - 1000°C, inert gas.
- (2) Increased ability of the products to decompose peroxide.
- (3) Effective peroxide reduction → (i) protection of the catalyst against degradation, (ii) shift in the ORR mechanism towards the 4e<sup>-</sup> pathway.
- (4) Degradation of the original structure and formation of highly condensed phases at high temperatures ( $T > 400^\circ\text{C}$ ).



**Pyrolysis products:** (i) unchanged macrocycle, (ii) polymers with different degree of polymerization, (iii) smaller compounds of  $\text{N}_4$  structure, (iv) products consisting of C, N, and metal atoms, (v) metal oxides, (vi) metal carbides, and (vii) metal phases.

# High-Resolution Transmission Electron Microscopy

## Key Role of Silica



*Well-dispersed, porous and “self-supported” pyropolymer left after KOH etch*

# Experimental

## Cathode, Anode, Fuel Cell Testing

- **Catalyst synthesis** (University of New Mexico)
  - Silica-supported CoTPP, CoTMPP, Co/Fe(1:1)TPP \*)
  - Pyrolysis at 600 – 700°C in inert gas atmosphere
  - Silica support etched in KOH

- **Membrane-electrode assembly** (5 cm<sup>2</sup>)

*Cathode: 2 mg cm<sup>-2</sup>; pyrolyzed-porphyrin catalyst mixed with carbon black and recast Nafion<sup>®</sup>*

*Anode: 6 mg cm<sup>-2</sup> Pt black*

*Membrane: Nafion<sup>®</sup> 117*

- **Fuel-cell test conditions**

*Cathode: Air or oxygen, 30-psig or 0-psig backpressure*

*Anode: H<sub>2</sub>, 30-psig or 0-psig backpressure*

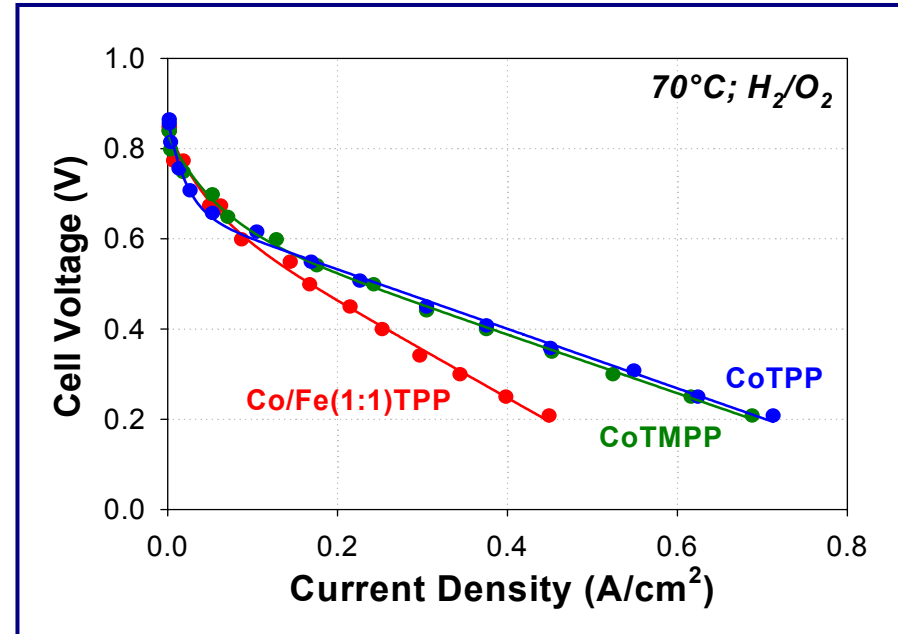
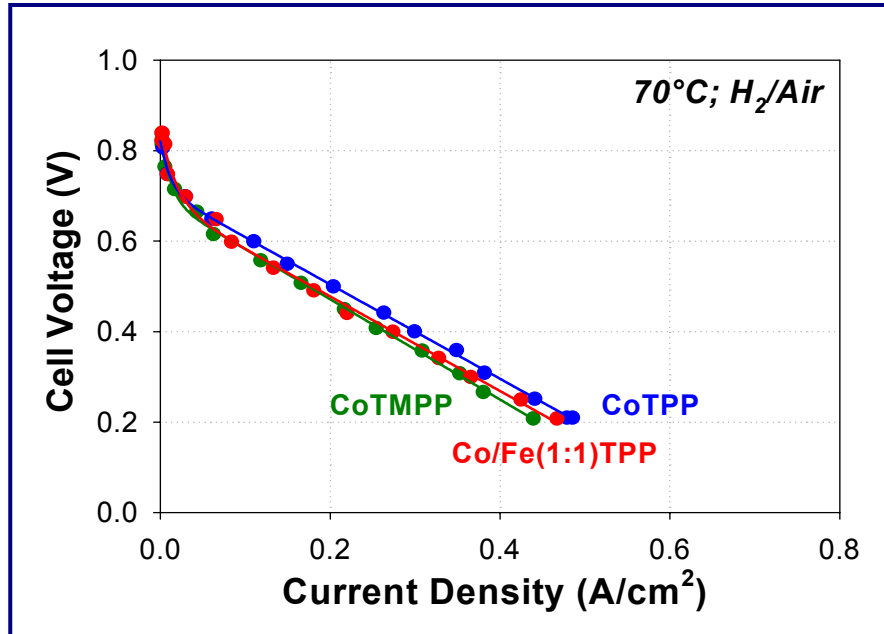
*Cell temperature: 30°C, 50°C, 70°C, and 80°C*

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*\*) TPP = tetraphenyl porphyrin; TMPP = tetramethoxyphenyl porphyrin*

# Performance at a Glance

## Remarkable Oxygen Reduction Activity

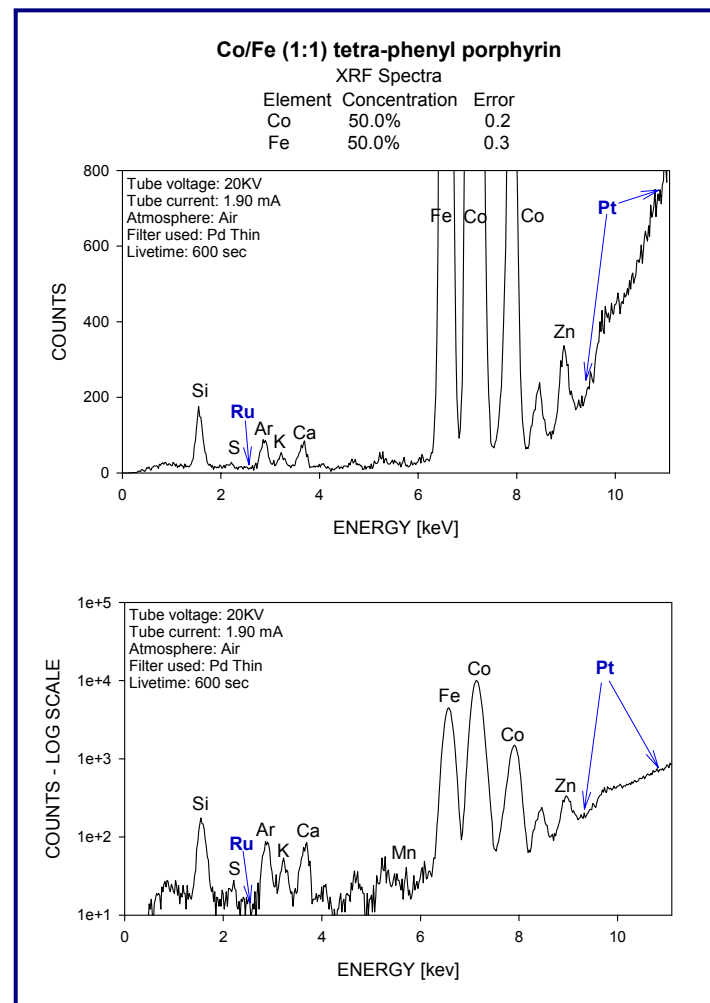
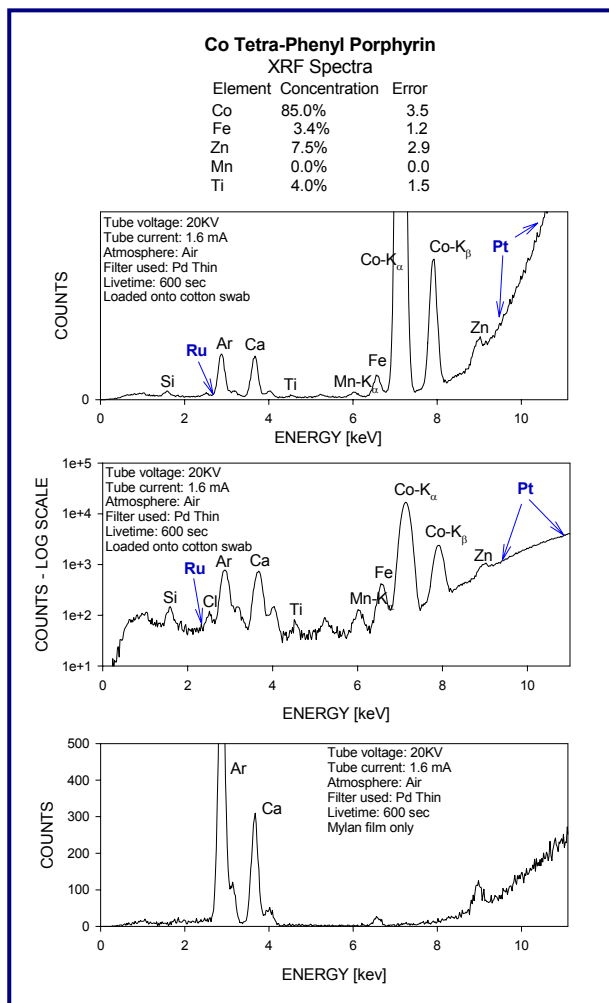


- **HIGHLIGHT:** Demonstrated high catalytic activity of three metalloporphyrins in H<sub>2</sub>-air and H<sub>2</sub>-O<sub>2</sub> fuel cells
- Similar performance observed with all catalysts when cathode operated on air
- Diminished performance of Co/Fe(1:1)TPP when exposed to oxygen at high temperature – possible oxidative loss of Fe



# X-Ray Fluorescence (XRF)

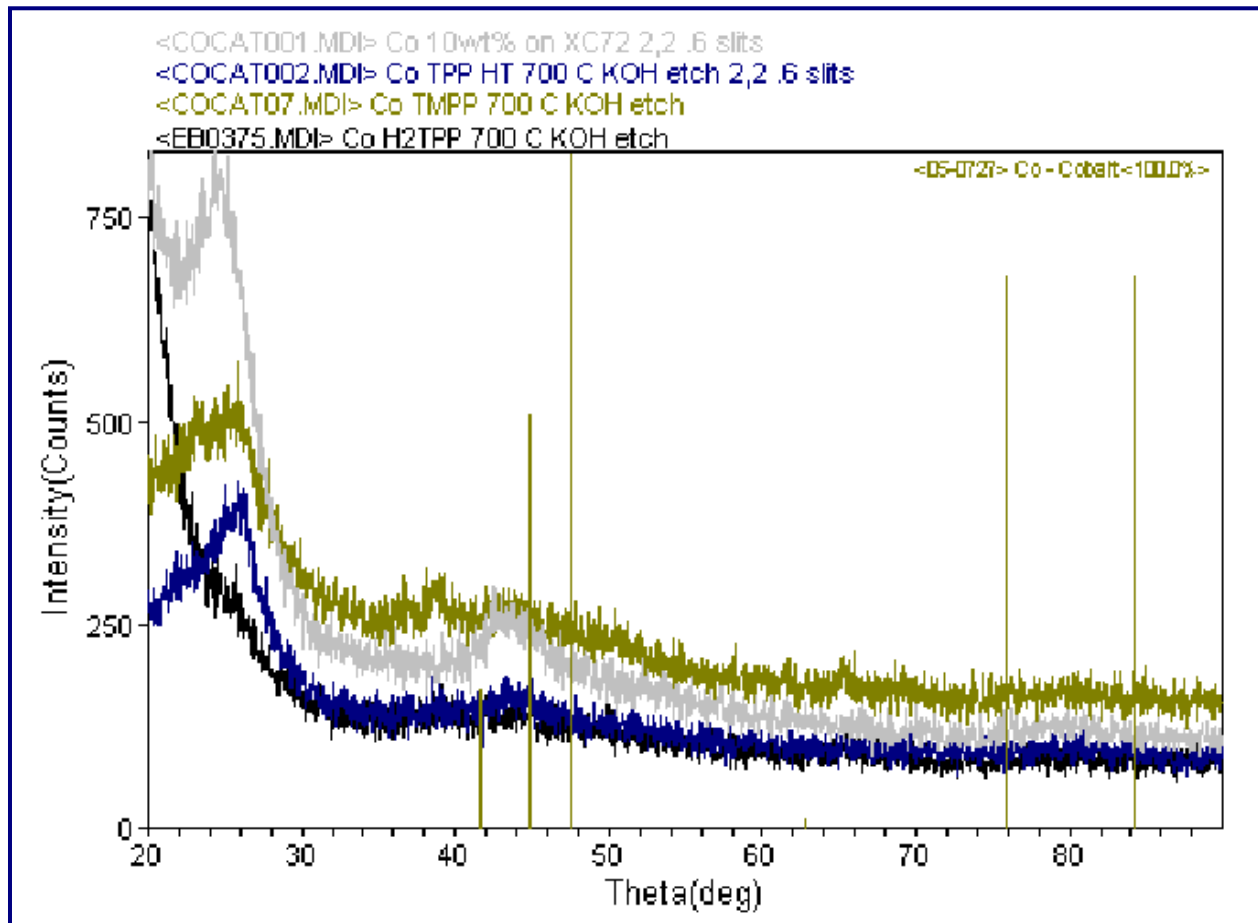
## No Traces of Noble Metals Detected



**No traces of Pt and Ru in CoTPP and Co/Fe(1:1)TPP catalysts**

# X-Ray Diffraction (XRD)

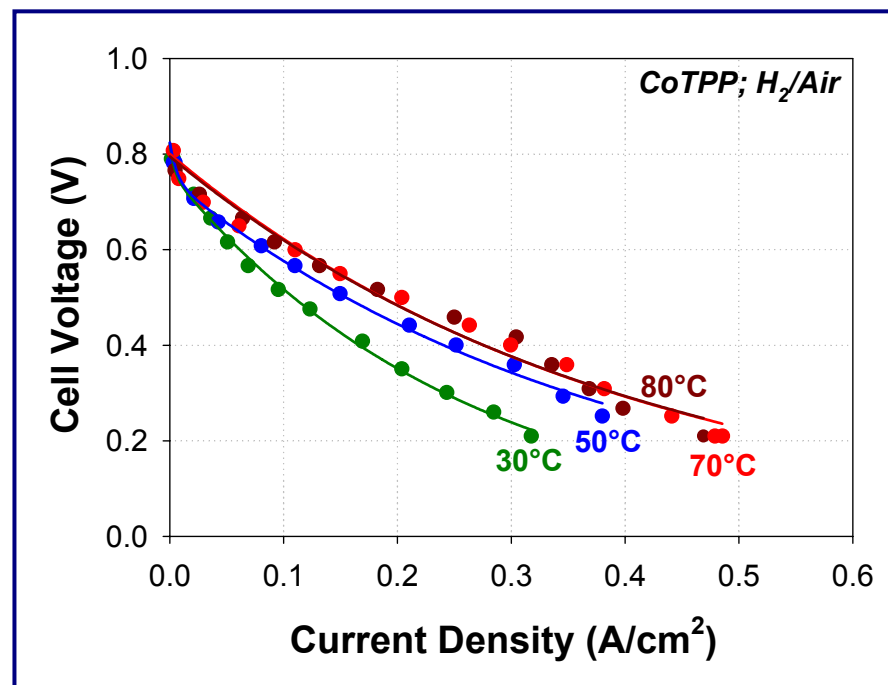
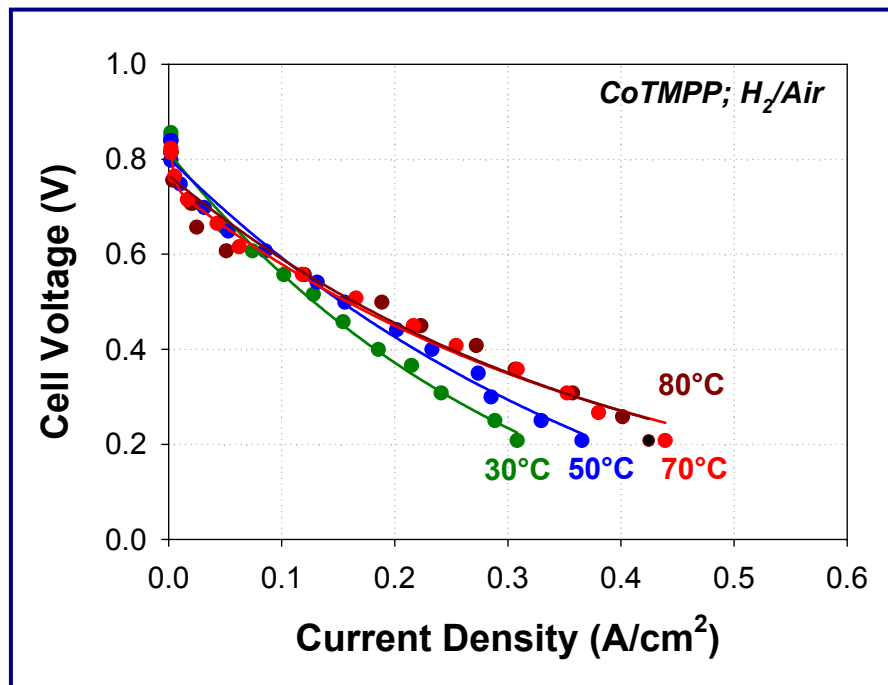
## Is Metallic Co a Factor?



**HIGHLIGHT:** Crystalline metallic Co absent in all cobalt-based catalysts – Co not a factor in ORR catalysis

# Catalyst Activity

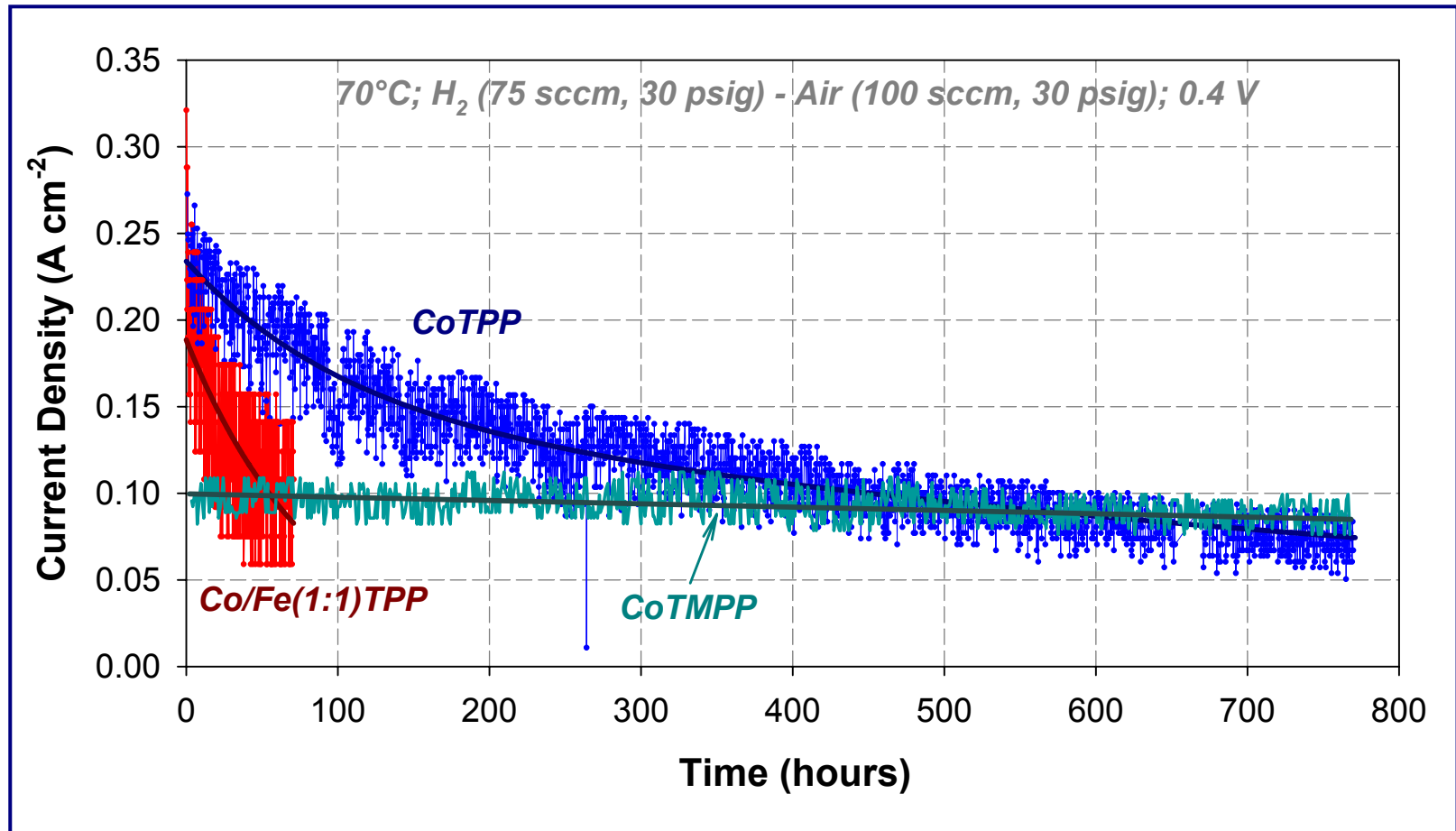
## Does the Porphyrin Type Matter?



- **Similar activity of CoTTP and CoTMPP cathodes at lower temperatures**
- **Slight initial performance advantage of CoTPP catalyst at higher temperatures**
- **Cathode structure may need further optimization**

# Durability

## Initial Performance vs. Performance Stability

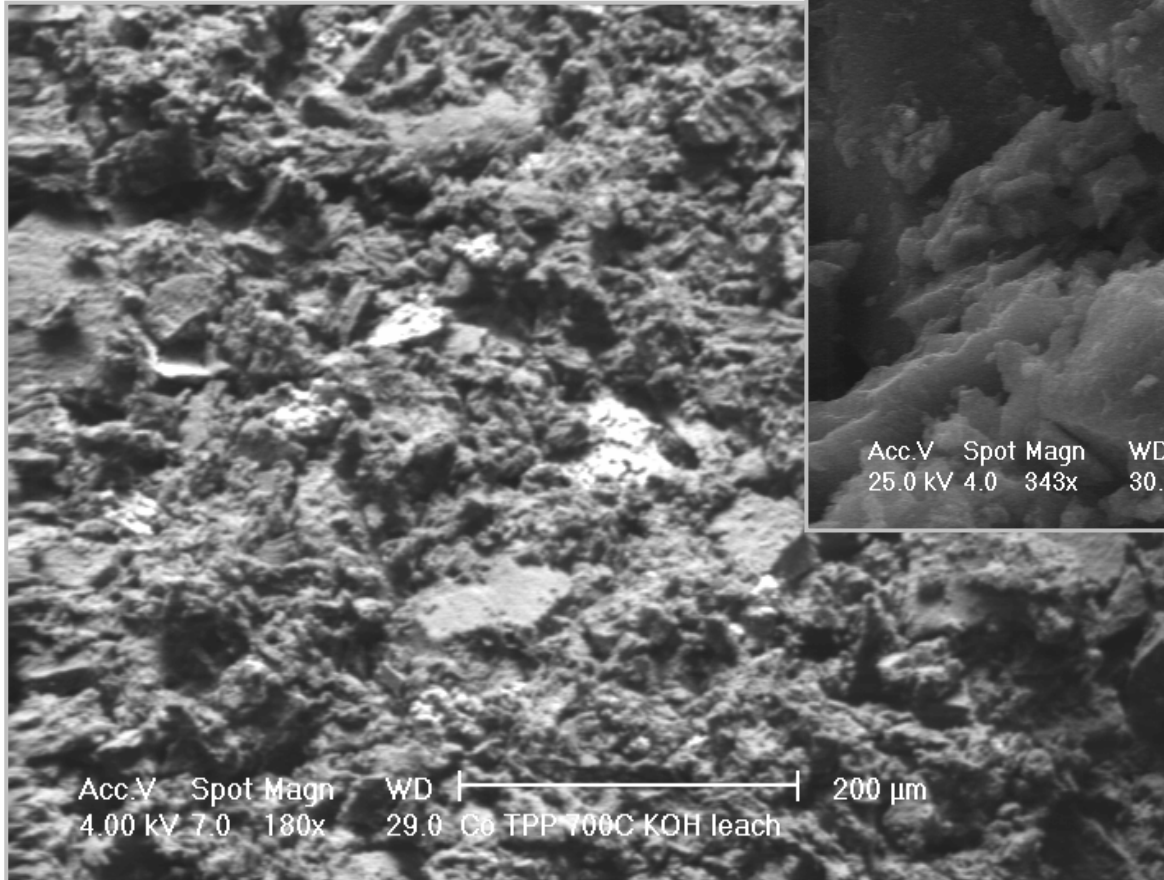


- **CoTPP** – the highest initial performance
- **CoTMPP** – the best long-term performance stability

# Active Reaction Site

## Scanning Electron Microscopy (SEM)

**SEM images of CoTPP catalyst at  
180 $\times$  and 343 $\times$  magnifications**

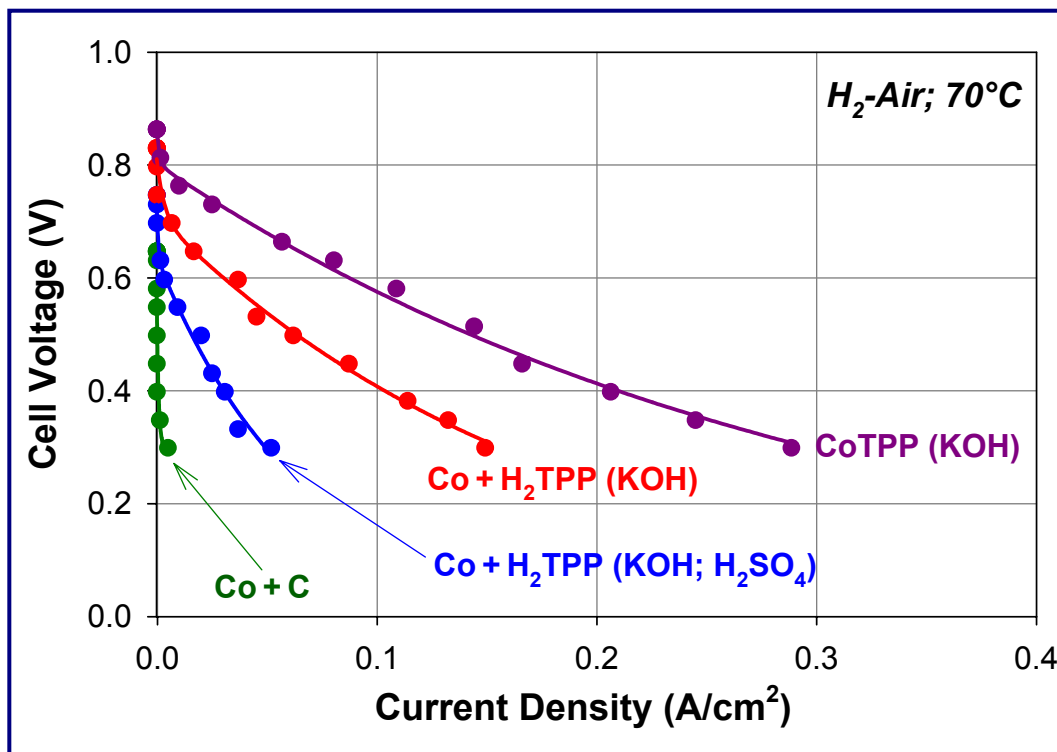


***Highly non-homogeneous  
catalyst morphology***

# Active Reaction Site

## Source of Catalytic Activity

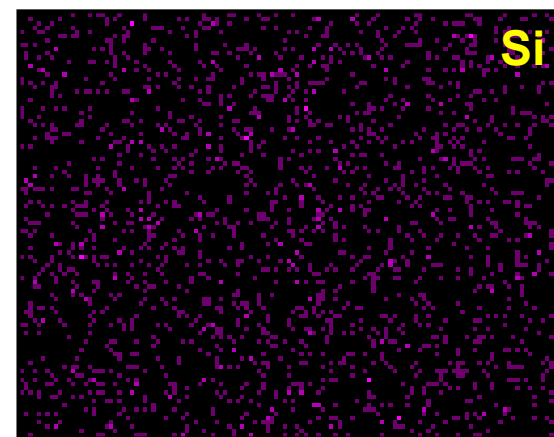
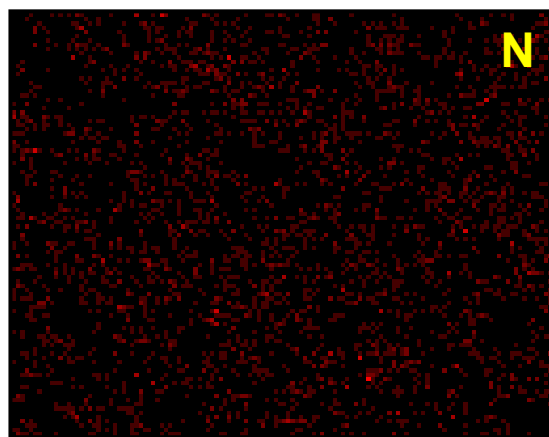
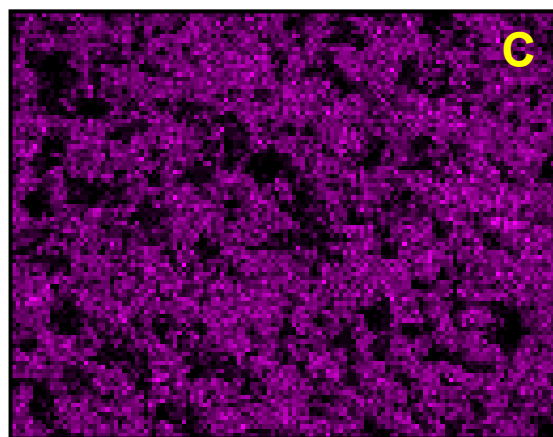
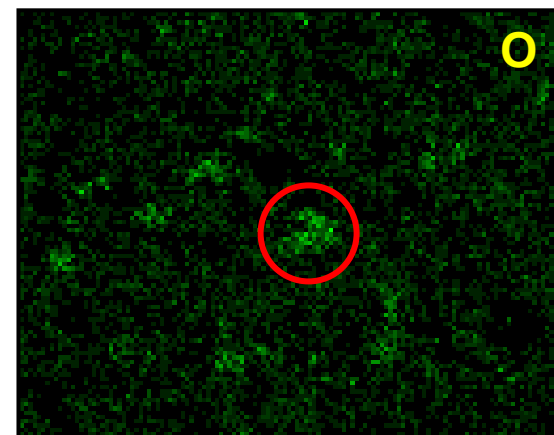
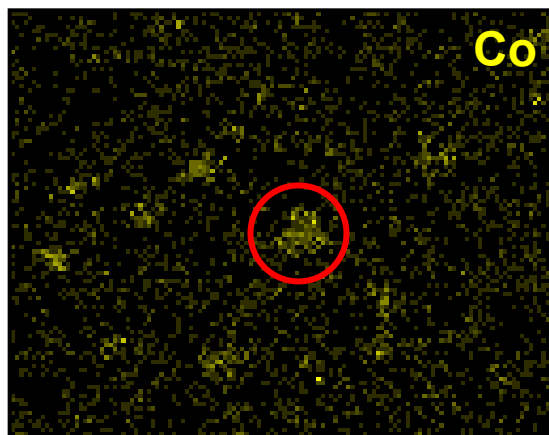
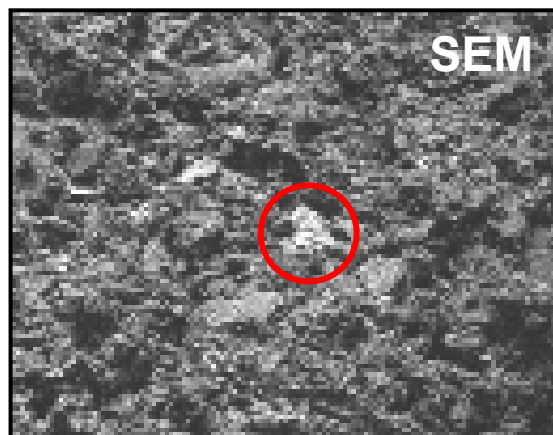
- Carbon-supported Co
- 10% Co + 90% H<sub>2</sub>TPP (HT 700°C, KOH etch, H<sub>2</sub>SO<sub>4</sub> bath)
- 10% Co + 90% H<sub>2</sub>TPP (HT 700°C, KOH etch)
- Co-TPP (HT 700°C, KOH etch)



**HIGHLIGHT:** Cobalt species, not N<sub>4</sub>-sites, appear to play major role in oxygen reduction at the CoTPP electrocatalysts

# Active Reaction Site

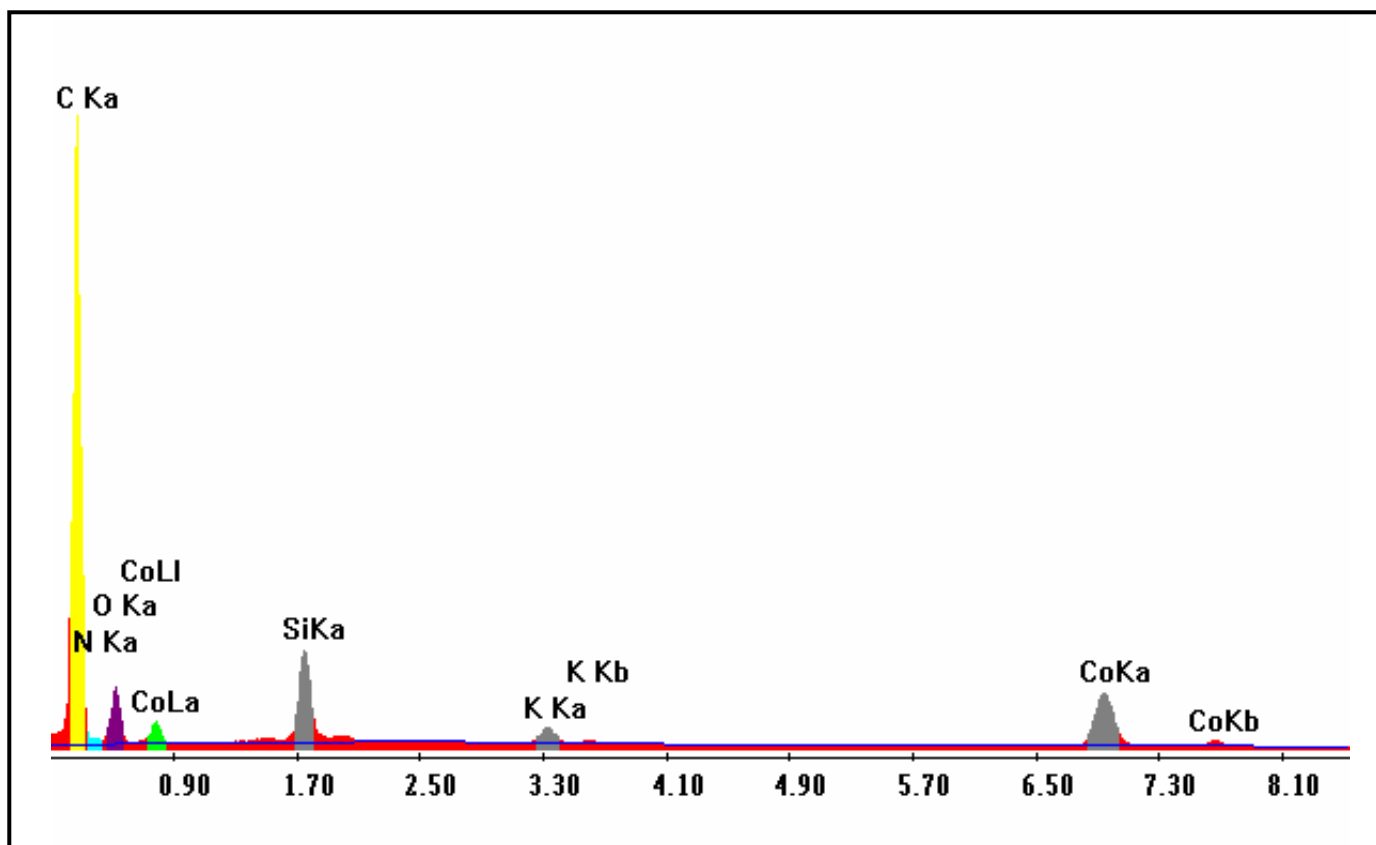
## EDX Mapping of CoTPP Catalyst



- **HIGHLIGHT:** Excellent correlation in the distribution of cobalt and oxygen
- Nitrogen distributed uniformly, not correlated with cobalt or oxygen
- Silicon (from remaining silica) and potassium (from KOH) uniformly distributed

# Active Reaction Site

## EDX Spectrum of CoTPP Catalyst

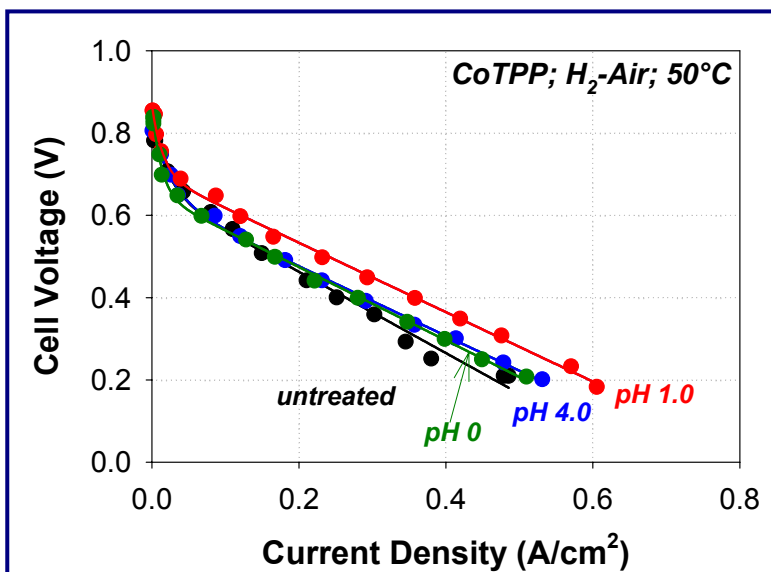
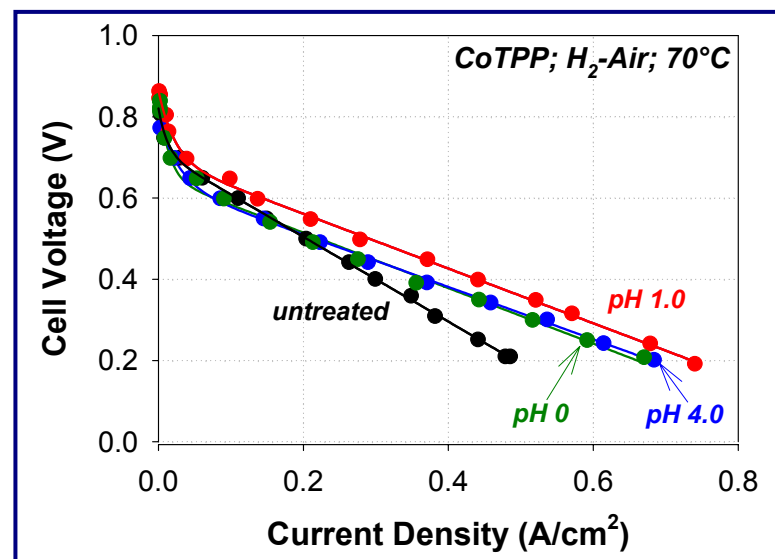
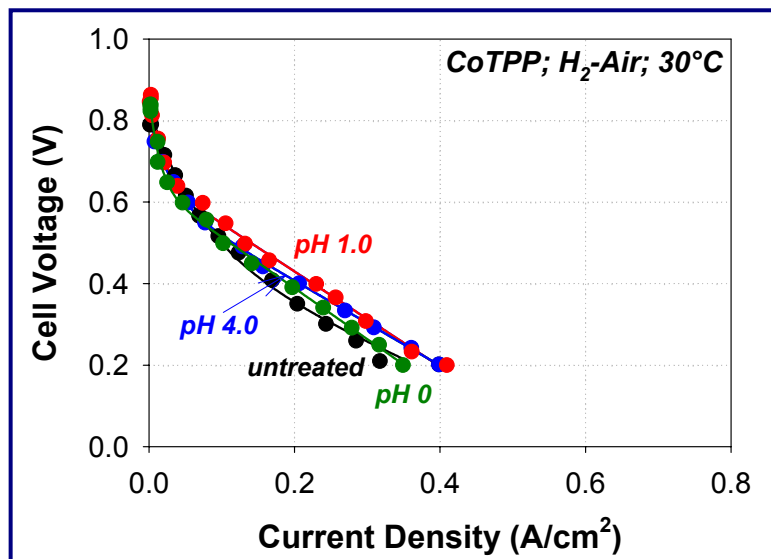


- **HIGHLIGHT:** Very little nitrogen relative to cobalt
- Noticeable presence of silicon and potassium
- Potential for further catalyst performance improvement via removal of Si and K



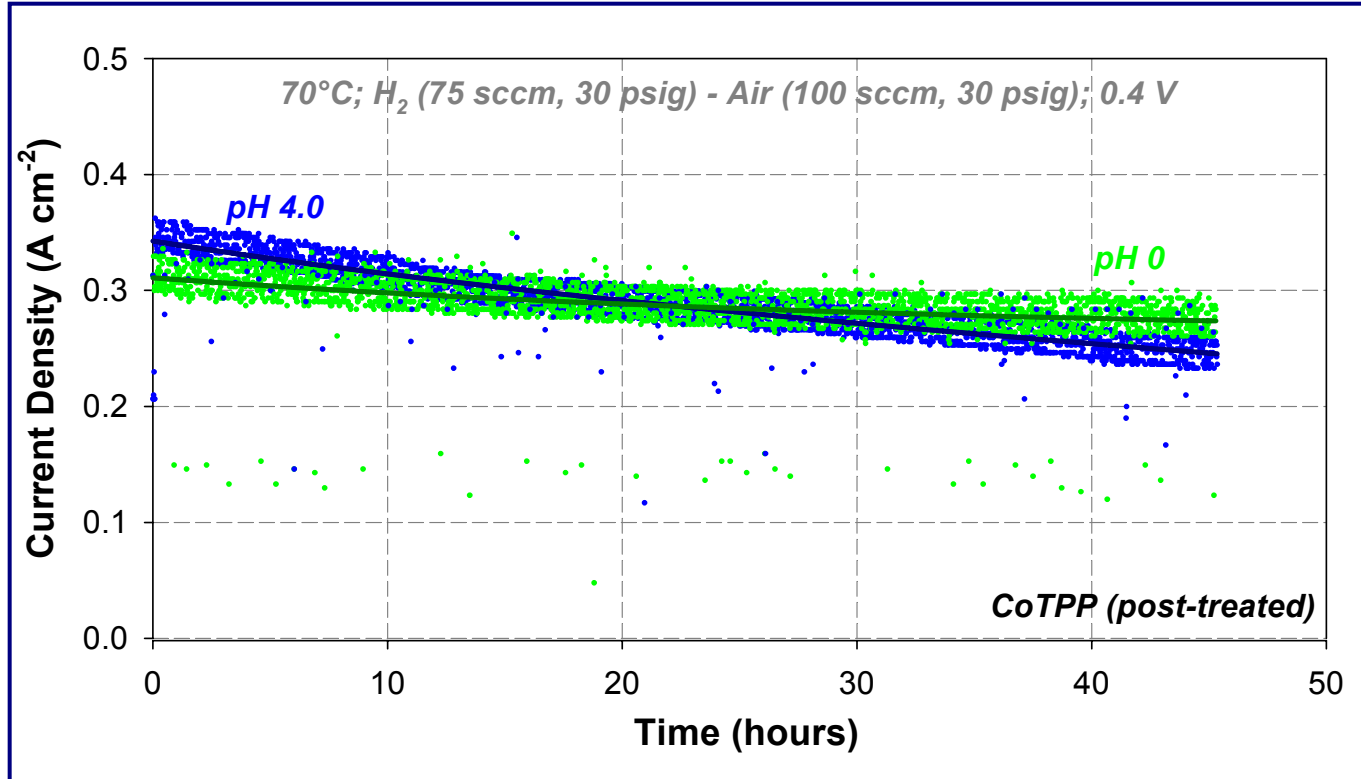
# Effect of pH

## Dilute Acid Post-Treatment of Catalyst Powders



- **HIGHLIGHT:** Post-treatment with dilute acid – a promising method of enhancing catalytic activity
- pH 1.0 treatment leading to the highest increase in catalytic activity, up to 100 mV at 50-70°C
- Improved air access due to the removal of inactive species – a likely reason for improved catalyst performance

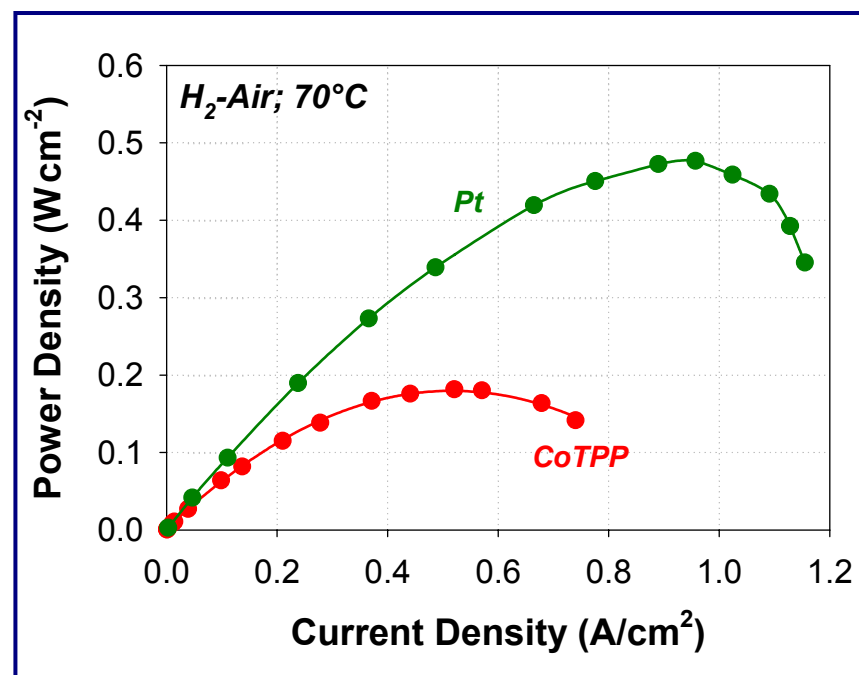
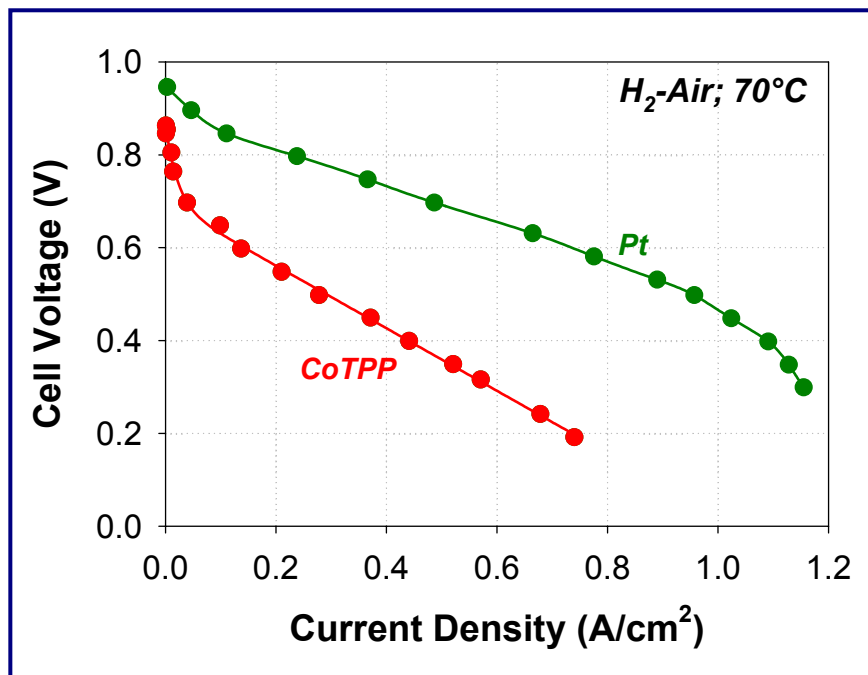
# Effect of pH Performance Stability



- **HIGHLIGHT:** pH treatment leading to significant gains in both short- and long-term performance of CoTPP catalyst
- CoTPP treated at pH 4.0 – good initial performer  
CoTPP treated at pH 0 – the most stable catalyst

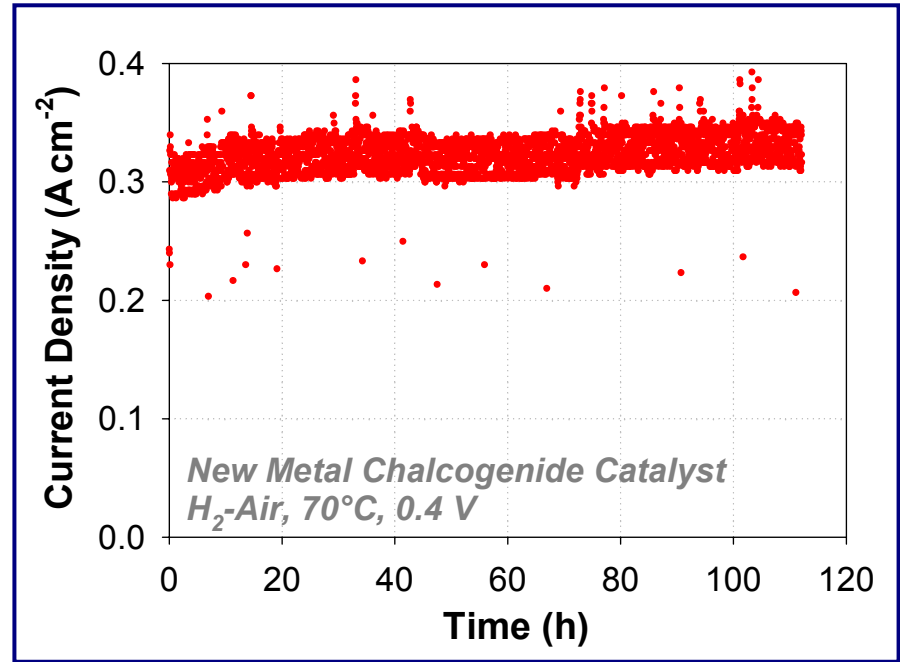
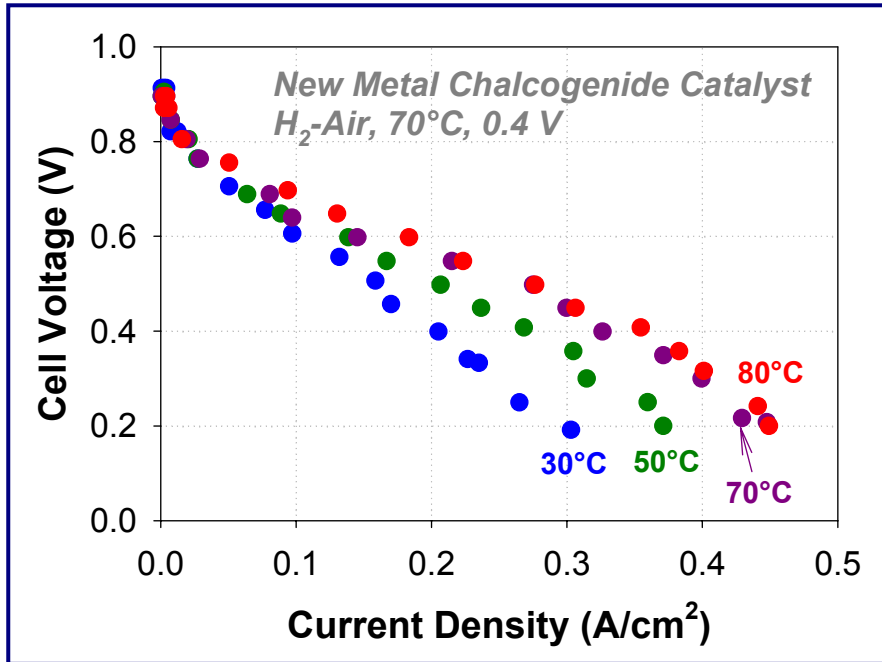
# Co-TPP vs. Pt at the Fuel Cell Cathode

## Performance Comparison



- **HIGHLIGHT:** *H<sub>2</sub>-air cell operated with a post-treated CoTPP cathode capable of delivering up to 0.180 W cm<sup>-2</sup>, ca. 1/3 of the cell with a Pt cathode at the same loading (2 mg cm<sup>-2</sup>)*
- *In addition to further improvements in the activity and stability of metalloporphyrin catalysts, an increase in operating potential, by as much as 100 mV, is needed for better efficiency*

# The Latest Metal Chalcogenides

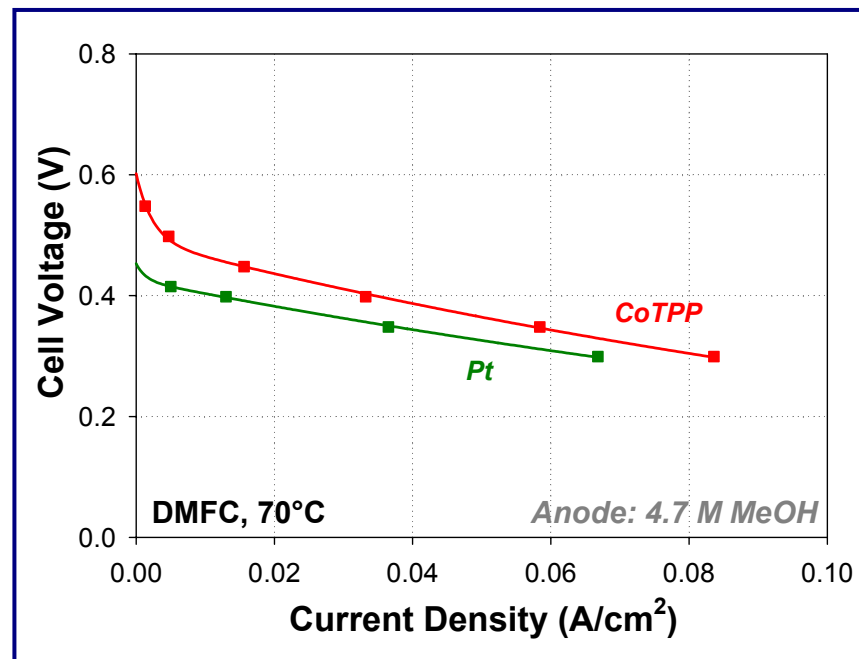
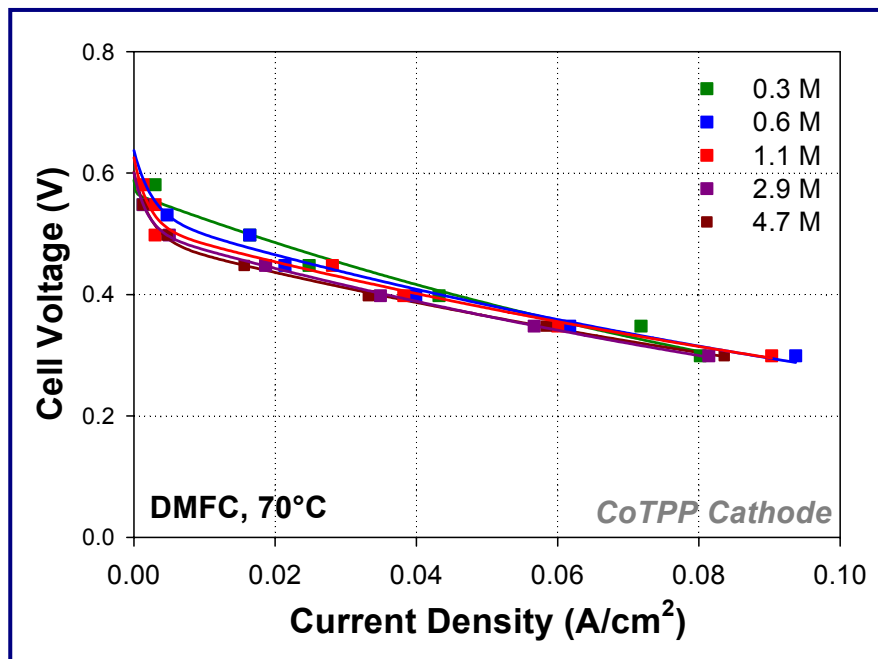


**HIGHLIGHT:** *New chalcogenide catalyst exceeding the performance of best post-treated metalloporphyrins without any performance drop over the first **110 hours!***

© *Collaboration with Université de Poitiers and University of Illinois*

# Additional Benefit

## Crossover Methanol Tolerance



- **HIGHLIGHT:** Very good methanol tolerance of CoTPP cathode catalyst in cells with up to ~5 M methanol concentration in the anode feed stream
- Non-precious metal catalyst outperforming Pt black catalyst (2 mg cm<sup>2</sup> loading) in cells with high MeOH anode concentration
- **HIGHLIGHT:** New metal chalcogenide catalyst found tolerant up to 17 M methanol

## Progress Towards Milestones

- *Develop techniques for electrochemical characterization of non-precious metal catalysts under conditions relevant to fuel cell operation (June 2004).*

**Milestone fully achieved** – Implemented electrochemical techniques: **(i)** fuel cell testing: hydrogen-air, DMFC; **(ii)** rotating disk electrode (RDE) & rotating ring-disk electrode (RRDE); **(iii)** ultramicroelectrodes.

- *Perform initial electrochemical/pH stability experiments on pyrolyzed macrocycle transition metal (PMTM) catalysts (March 2005).*

**Milestone achieved & exceeded** – Performance stability determined with three different metalloporphyrin catalysts; effect of acidity on initial and long-term performance of catalysts studied at three pH values used in “post-treatment”.

- *Identify active reaction site(s) for oxygen reduction on pyrolyzed  $N_4$ -chelate electrocatalyst in polymer electrolyte fuel cell (September 2005).*

**Milestone on schedule** – Results obtained to date make  $N_4$ -site questionable as the active reduction center; good correlation between cobalt and oxygen distribution points to major role of cobalt oxides (hydroxides).

# Research Plans

## Remainder of FY 2005

- *Identify and characterize the active site (or sites) for oxygen reduction reaction (ORR) at the metalloporphyrin surface.*

## FY 2006 Objectives

- *Determine distribution of active ORR sites on the surface of metalloporphyrins as a function of (i) catalyst type, (ii) fabrication technique and conditions, (iii) catalyst “post-treatment” (including in-depth determination of the effect of solution pH).*
- *Investigate structures potentially leading to the protection of active ORR site(s) in acidic media and thus improved activity and durability of metalloporphyrin catalysts.*
- *Lower high-frequency resistance of membrane-electrode assemblies with non-precious metal cathode catalysts.*
- *Perform performance study of metal chalcogenides as very promising alternatives to metalloporphyrins.*

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## **Non-Precious Metal Catalysts (Supplement)**

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# Conference Presentations

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1.205th Meeting of the Electrochemical Society, San Antonio, Texas, May 9 – 13, 2004. Title: “Non-Platinum Electrocatalysts for Polymer Electrolyte Fuel Cells: Fuel Cell Evaluation of Oxygen Reduction Catalyst” S. Levendosky, P. Atanassov, J. Davey and P. Zelenay.

2.206th Meeting of the Electrochemical Society, Honolulu, Hawaii, October 3 – 8, 2004. Title: “Non-Platinum Electrocatalysts for Polymer Electrolyte Fuel Cells: Methanol-Tolerant Cathode Catalyst,” S. Levendosky, P. Atanassov, B. Piela and P. Zelenay.

# Hydrogen Safety

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**The most significant hydrogen hazard associated with this project is:**

***Leak in the hydrogen supply resulting in accumulation of the gas in the room, which could then lead to explosion upon ignition.***

# Hydrogen Safety

**Our approach to dealing with this hazard is as follows:**

- Hydrogen sensors, interlocked with the hydrogen gas supply, have been installed in the laboratories with hydrogen supply from gas cylinders or from a hydrogen generator.***
- Hydrogen sensors have been installed at just below the ceiling where gas accumulation is most severe; also, two sensors are installed in every room for redundancy; the alarm is set off at 10% of Lower Flammability Limit (LFL).***
- In laboratories that use bottled hydrogen, only a single cylinder is used at any given time; the cylinder size is limited to ensure that the LFL is not exceeded even upon complete release of a full cylinder.***
- All work has been reviewed and approved through Los Alamos National Laboratory's safety programs:***
  - Hazard Control Plan (HCP) - hazard based safety review***
  - Integrated Work Document (IWD) - task based safety review***
  - Integrated Safety Management (ISM)***