



Fermentative Approaches to Hydrogen Production

**Pin-Ching Maness, Stefan Czernik and
Sharon Smolinski**

National Renewable Energy Laboratory

DOE HFC&IT Program Review

May 24, 2005

Project ID # PD18

This presentation does not contain any proprietary or confidential information



Overview

Timeline

- Project start date: FY 05
- Project end date: on going
- Percent complete: NA

Budget

- Total project funding
 - \$200K (DOE share)
- Funding received in FY04: \$0.00
- Funding for FY05: \$200K

Barriers

- Production Barriers addressed
 - Barrier AI: H₂ Molar Yield
 - Barrier AK: Feedstock Cost

Partners

- **Interactions/collaborations**
 - Dr. Bruce Logan, Dr. Jay Regan, Penn State University
 - Dr. Lee Lynd, Dartmouth College
 - Dr. David Levin, Univ. of Victoria (Canada)

Objectives

- The long-term goal is to assist DOE in developing direct fermentation technologies to convert renewable biomass resources to H₂
- The objectives in FY05 are to:
 - Screen and identify **cellulolytic microbes** which can produce H₂ directly from cellulose and hemicellulose, major constituents of biomass
 - Identify up to 3 suitable strains of fermentative microbes to select one from for pathway engineering to improve H₂ molar yield in FY06 and beyond (**FY05 Milestone**)

Approach to Address Feedstock Barrier (AK)

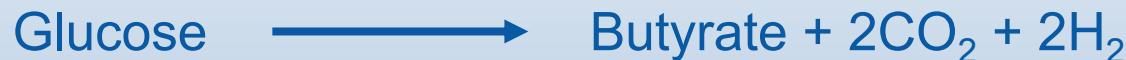
- **Problem:** Near 75 to 90% of lignocellulosic biomass is composed of sugars, ideal substrates for H₂ production. NREL's Biomass Program is developing technologies to lower the cost of glucose from biomass to 8 cents per pound by 2015

Component	% Dry Weight
Cellulose	40-60%
Hemicellulose	20-40%
Lignin	10-25%

- **Approach:** Bio-prospect cellulolytic microbes that can convert cellulose and hemicellulose (xylose) directly, in lieu of glucose, to H₂ as an alternative and valid strategy to lower the feedstock cost barrier

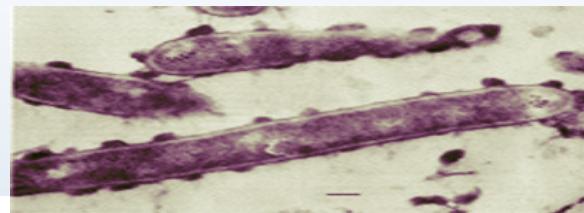
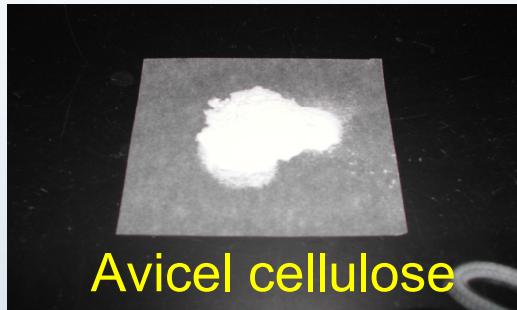
Approach to Address H₂ Molar Yield (AI)

- **Problem:** Molar Yield of H₂ (mol H₂/mol sugar) is too low (2 to 2.5) due to the simultaneous production of other fermentation waste byproducts

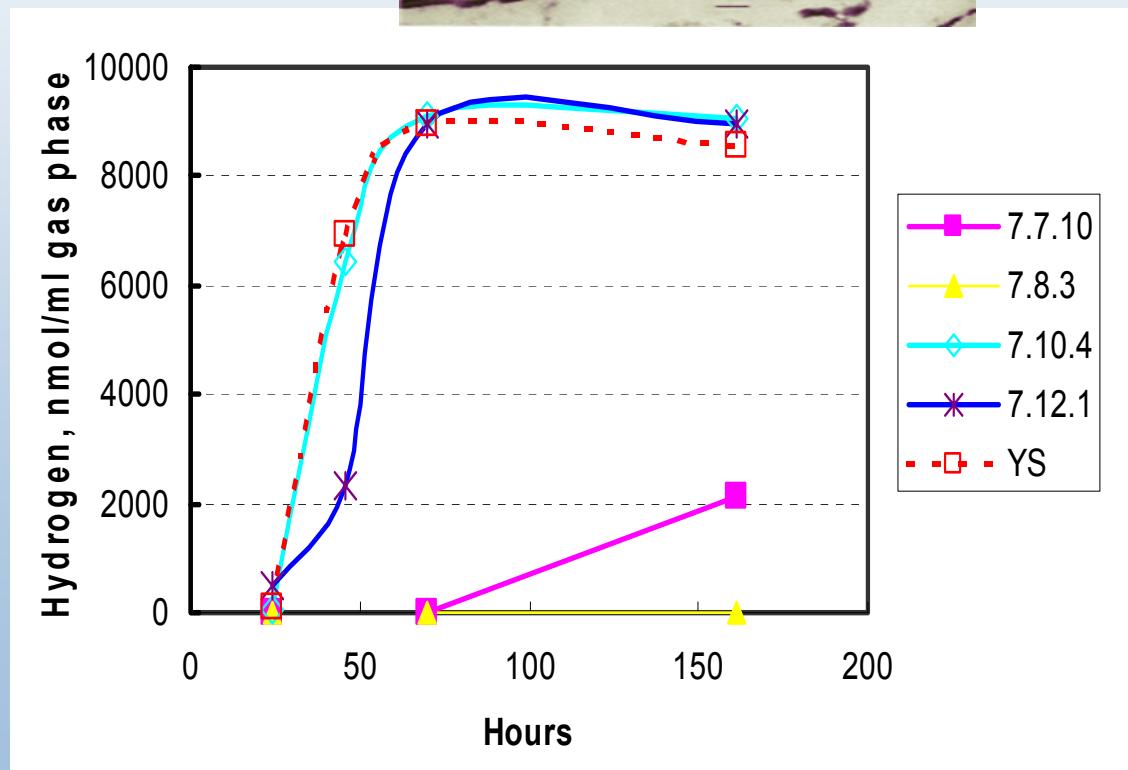


- **Approach (FY2006 and beyond):** Select a suitable cellulolytic microbe of known genome sequence for metabolic pathway engineering
 - Block competing pathways has been demonstrated in literature in improving H₂ molar yield

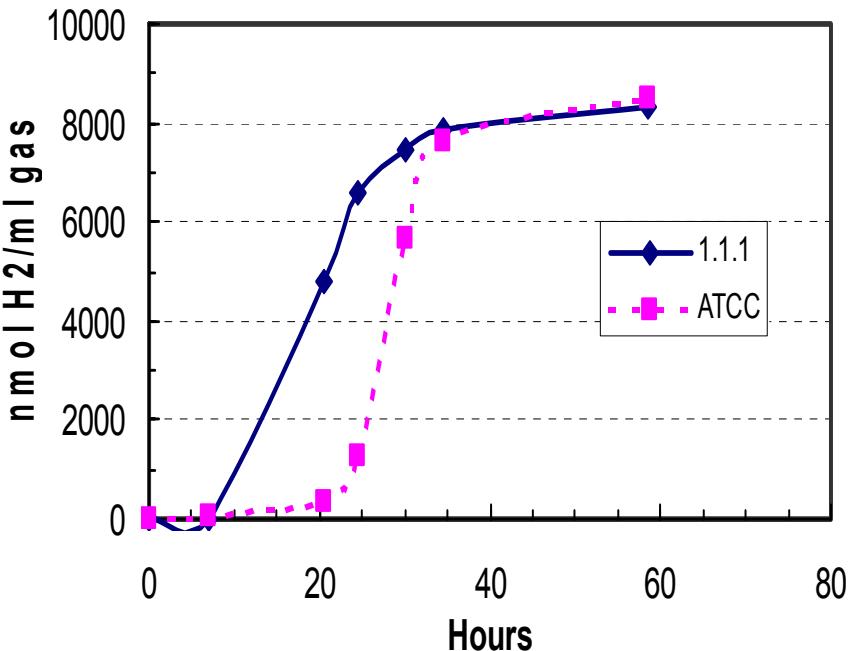
Technical Accomplishment/Progress – Screening 9 Strains of *Clostridium thermocellum*



- Avicel® is the most recalcitrant cellulose
- Fermentation was carried out at 55 °C
- H₂ production resumes when the headspace H₂ was displaced with an inert gas



Technical Accomplishment/Progress – Screening 9 Strains of *C. thermocellum*



- Cellulose utilization is noted by a change in color

Strains were kindly provided to us by Profs. Lee Lynd (Dartmouth College) and Ed Bayer (Weizmann Institute of Science, Israel)

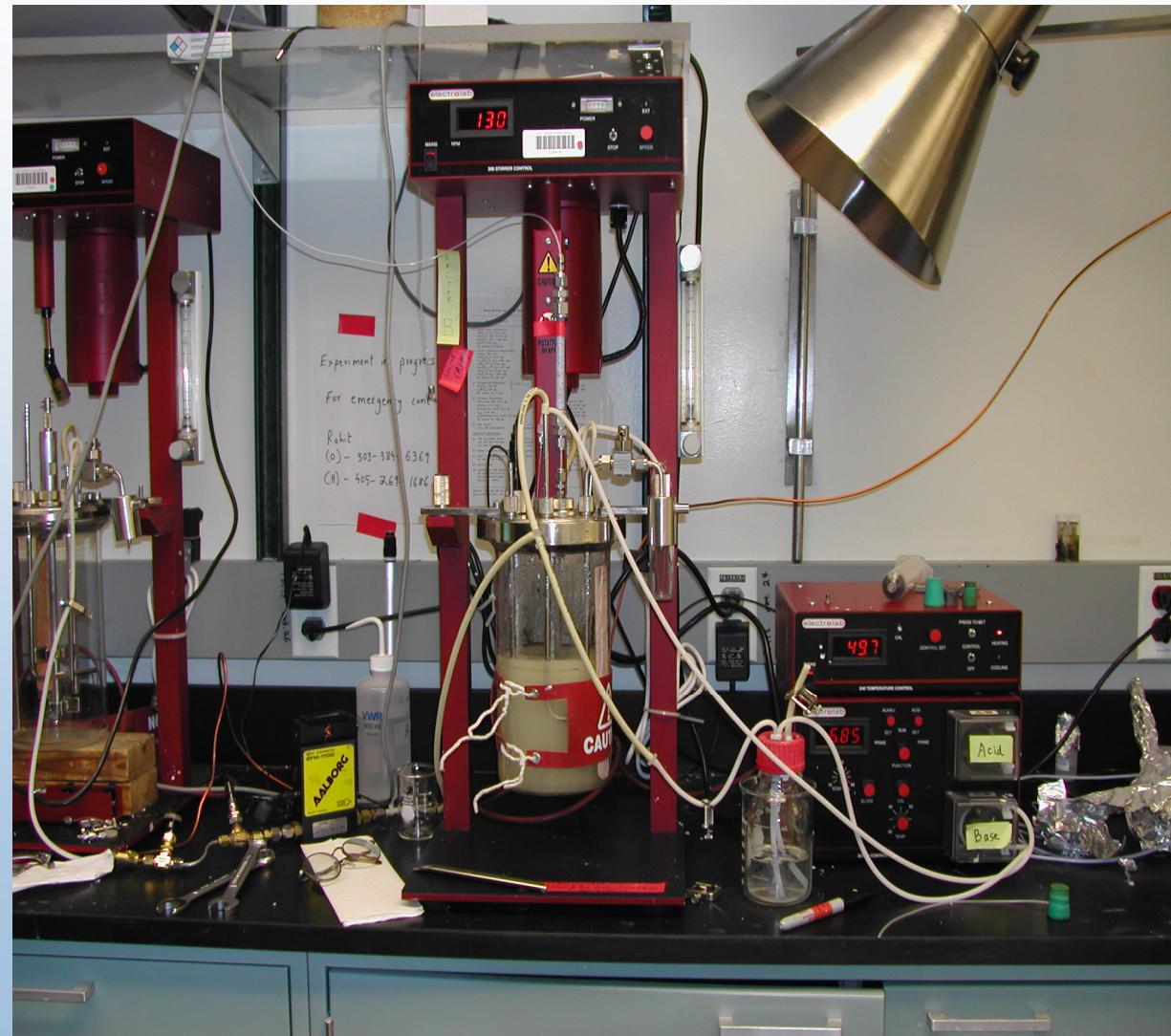
Technical Accomplishment/Progress – Identified the Suitable H₂ Producer

Strains	Rate of H ₂ Production*
ATCC	1018
1.1.1	595
YS	477
7.10.4	447
7.12.1	407
7.7.10	35
7.8.3	Traces
6.3.2	Traces
7.9.4	Traces

- Screened **9** strains of cellulolytic microbes
- ATCC strain has the highest rate. Work is underway to optimize its growth conditions to eliminate the lag phase
- **Strain 1.1.1** was selected for scale-up experiment due to its fast growth rate in **cellulose**
- Screening effort is ongoing
- **Using cellulose in lieu of glucose will meet the technical target of lowering the feedstock cost**

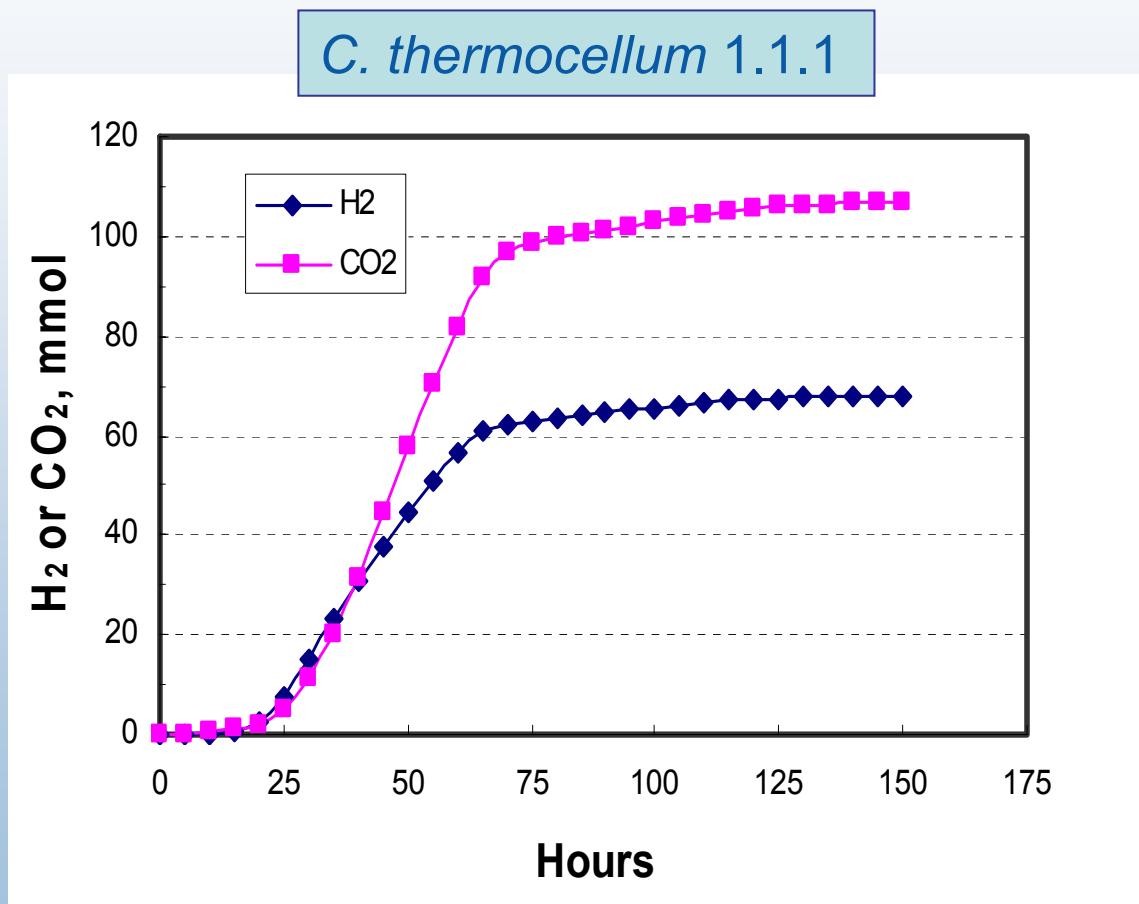
* nmol H₂/hr/ml culture gas phase

Bioreactor Configurations for Cellulose Fermentation



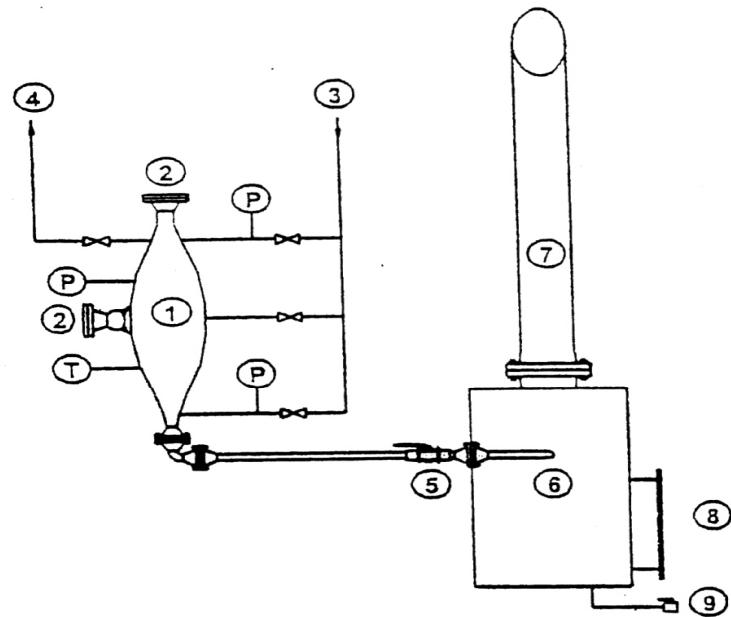
- pH and temperature controlled
- Operate two reactors simultaneously
- On-line continuous sampling of reactor gas phase via gas chromatography
- H₂/CO₂ is vented continuously, no pressure buildup

Technical Accomplishment/Progress: H_2 from Cellulose in Bioreactor



- 0.5% (w/v) Avicel was consumed completely
- Fermentation waste byproducts are ethanol, and acetic acid with traces of lactic and formic acids
- Carbon mass balance approaching 90%
- **H₂ molar yield near 2**
- **First demonstration of H₂ molar yield data from cellulose**

Corn Stover Pretreatment: Steam Explosion



1 - Pressure Vessel; 2 - MSW feeding; 3 - Steam line; 4 - Safety vent;
5 - Release valve; 6 - Receiver; 7 - Waste steam exhaust pipe;
8 - Exploded material withdrawal door; 9 - Liquid collection line;
T - Temperature gauge; P - Pressure gauge

Liu et al. 2002. Biotech Bioengineering 77: 121-130.



Corn Stover

Steam Explosion
(acid or neutral)

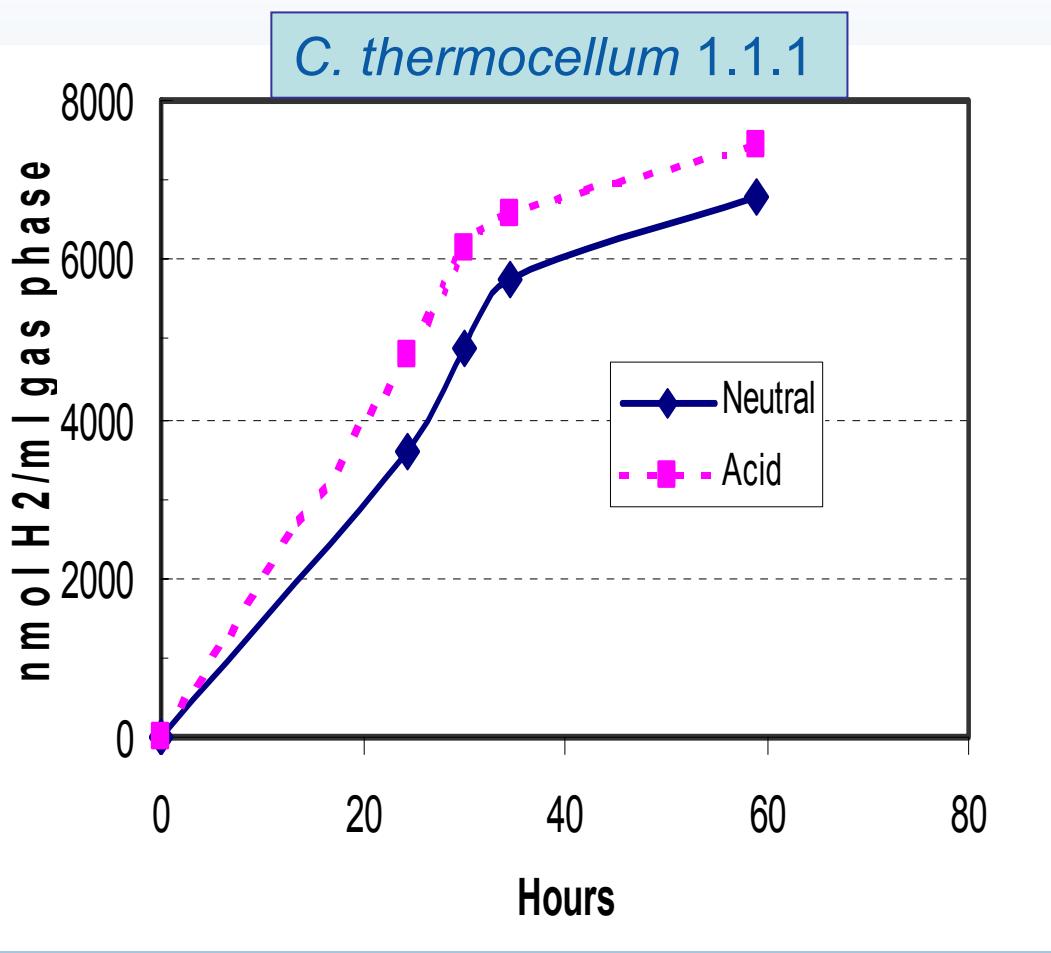
Aqueous
Hemicellulose

(5- and 6-carbon
sugar oligomers)

Solid
Lignocellulose
(cellulose & lignin)



Technical Accomplishment/Progress: H_2 from Corn Stover Lignocellulose Solids



Neutral: 220 °C, 3 min
Acid: 190 °C, 1 min



Solids before and after fermentation

➤ Near 93% and 86% of cellulose and hemicellulose were consumed, respectively.

Responses to Previous Year Reviewers' Comments

- This new project started Oct 1, 2004 and has not been reviewed previously

Future Work

- **Remainder of FY2005:**
 - Screen additional cellulolytic microbes such as *Clostridium cellulovorans*, *C. cellulolyticum*, etc.
 - Further optimize fermentation parameters in scale-up bioreactor
 - Determine carbon balance and H₂ molar yield
 - Identify the best microbe of known genome sequence for metabolic engineering in FY2006 (**FY2005 Milestone**)
- **FY2006:**
 - With the selected model microbe, conduct metabolic profiling to determine the most effective strategy to redirect biochemical pathways (**FY2006 Milestone**)
 - Begin genetic engineering to block competing pathways to improve molar yield of H₂

Publications and Presentations

- **Publications**

- Datar, R., J. Huang, P. C. Maness, A. Mohagheghi, S. Czernik, and E. Chornet. Hydrogen production from the fermentation of corn stover biomass pretreated with a steam explosion process. Submitted to Environ. Sci. Technol.
- Lee, J. Z., D. M. Klaus, P. C. Maness, and J. R. Spear. Characterization of the effect of butyrate on hydrogen production in photofermentation for use in Martian Resource Recovery. Submitted to Intl. J. Hydrogen Energy

- **Presentations**

- The 10th Annual Meeting of Institute of Biological Engineering, Athens, GA. March 2005
- Graduate Student Seminar Series, Dept. of Civil & Environ. Engineering, Penn State University, PA. April 2005

Hydrogen Safety

- The most significant hydrogen hazard associated with this project is the use of H₂-containing anaerobic glovebox for sample preparations under anaerobic environment
 - Anaerobic glovebox routinely contains 2-3% H₂ (in N₂), provided via a 10% H₂ gas cylinder (in N₂)
 - Inside glovebox are small electrical devices and power cords needed for sample preparations

Hydrogen Safety

- Our approaches to deal with this hazard are:
 - Install H₂/O₂ gas monitor inside the glovebox, with alarms set at 10% H₂ and 300ppm O₂ (Factory preset)
 - Maintain H₂ level inside the glovebox at 2-3% (in N₂)
 - Activate palladium catalyst frequently
 - The power cord is unplugged from the mains (outside) first prior to any (dis)connection inside the glovebox
 - Use a flammable gas detector to detect potential H₂ leaks out from the glovebox
 - NREL laboratory ventilation system provides 6 to 10 complete air exchanges per hour in the event of a catastrophic leak
 - The DOE Hydrogen Safety Review Team visited NREL in 2004 and we have incorporated their suggestions in our AOP.