



# Low Temperature Electrolytic Hydrogen Production

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This presentation does not contain any proprietary or confidential information

Project ID  
#PDP56



# Overview

## Timeline

- July 1, 2004
- December 31, 2005
- 60%

## Budget

- Total project funding
  - DOE Share: \$244,693
  - Contractor share: \$0
- Funding received in FY04: \$244,693
- Funding for FY05: \$0

## Barriers

- Barriers addressed
  - Energy Efficiency
  - System Cost
  - Robust Materials

## Partners

- Savannah River National Laboratory: William Summers
- Argonne National Laboratory: Richard Doctor
- Idaho National Laboratory: Michael Simpson



# Objectives

Assist DOE in developing highly efficient, cost affective thermochemical cycles for H<sub>2</sub> production. Our focus is on the electrochemical step used in a variety of thermochemical cycles (*e.g.*, hybrid sulfur, modified Ca-Br).



# Approach

- Develop a *gas phase* proton exchange membrane (PEM) electrolyzer to convert HBr to Br<sub>2</sub> and SO<sub>2</sub> to H<sub>2</sub>SO<sub>4</sub>
- Quantify the relationships among design and operating parameters.

Our unique gas-phase process has significantly lower mass-transfer resistance that will provide:

- Higher current densities (*i.e.*, lower electrolyzer cost)
- Better thermal management (*i.e.*, higher efficiencies)
- Lower voltages (*i.e.*, higher efficiencies)
- Lower reactant crossover (*i.e.*, reduce poisoning providing longer life)
- Better control of product purity (*i.e.*, higher efficiencies)
- Lower catalyst loadings (*i.e.*, lower electrolyzer cost)



# Key Measurements

- Voltage → Electrical Energy and Efficiency
- Current Density → Electrolyzer Size  
(*i.e.*, capital costs)
- Outlet Concentration → Separation Cost  
and Efficiency
- Voltage Drift → Replacement Costs



# Operating Parameters

- Current
- Temperature
- Pressure
- Anode feed flow rate
- Anode feed composition
- Acidity of cathode feed

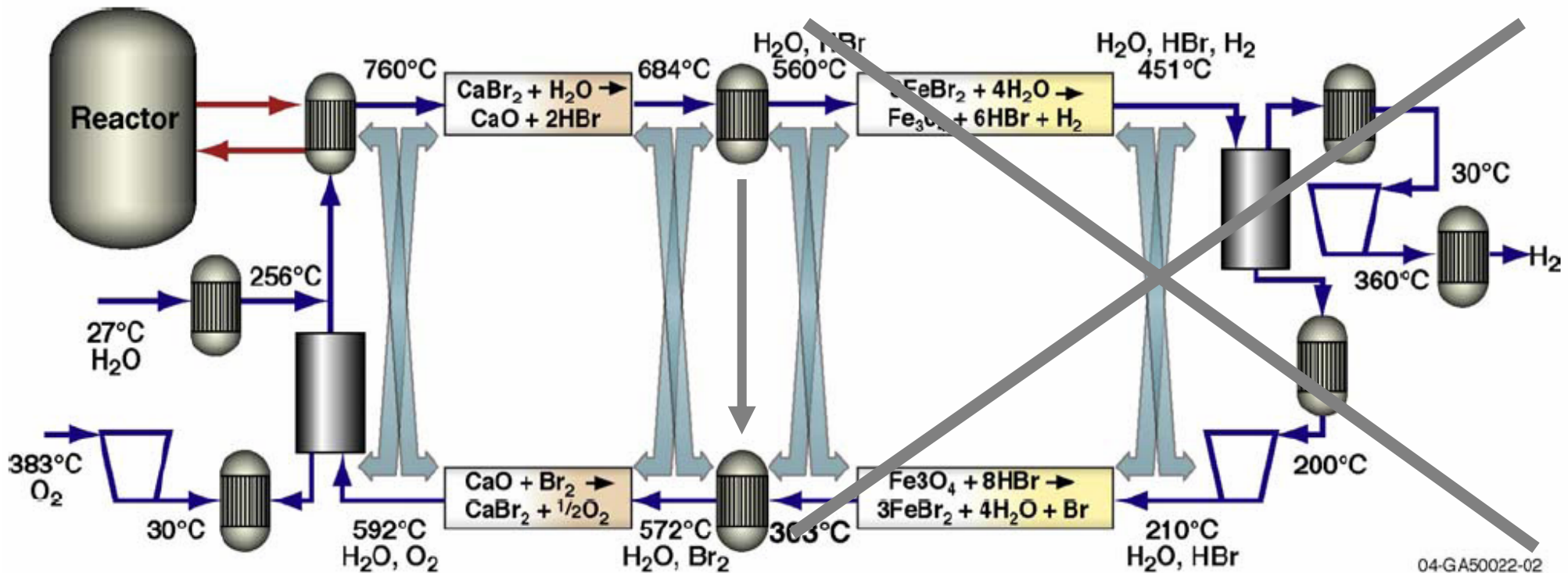


# Design Parameters

- Catalyst type and loading
  - Electrolyzer Costs
  - Voltage
  - Poisoning
- Membrane type and thickness
  - Voltage
  - Poisoning
  - Water Management



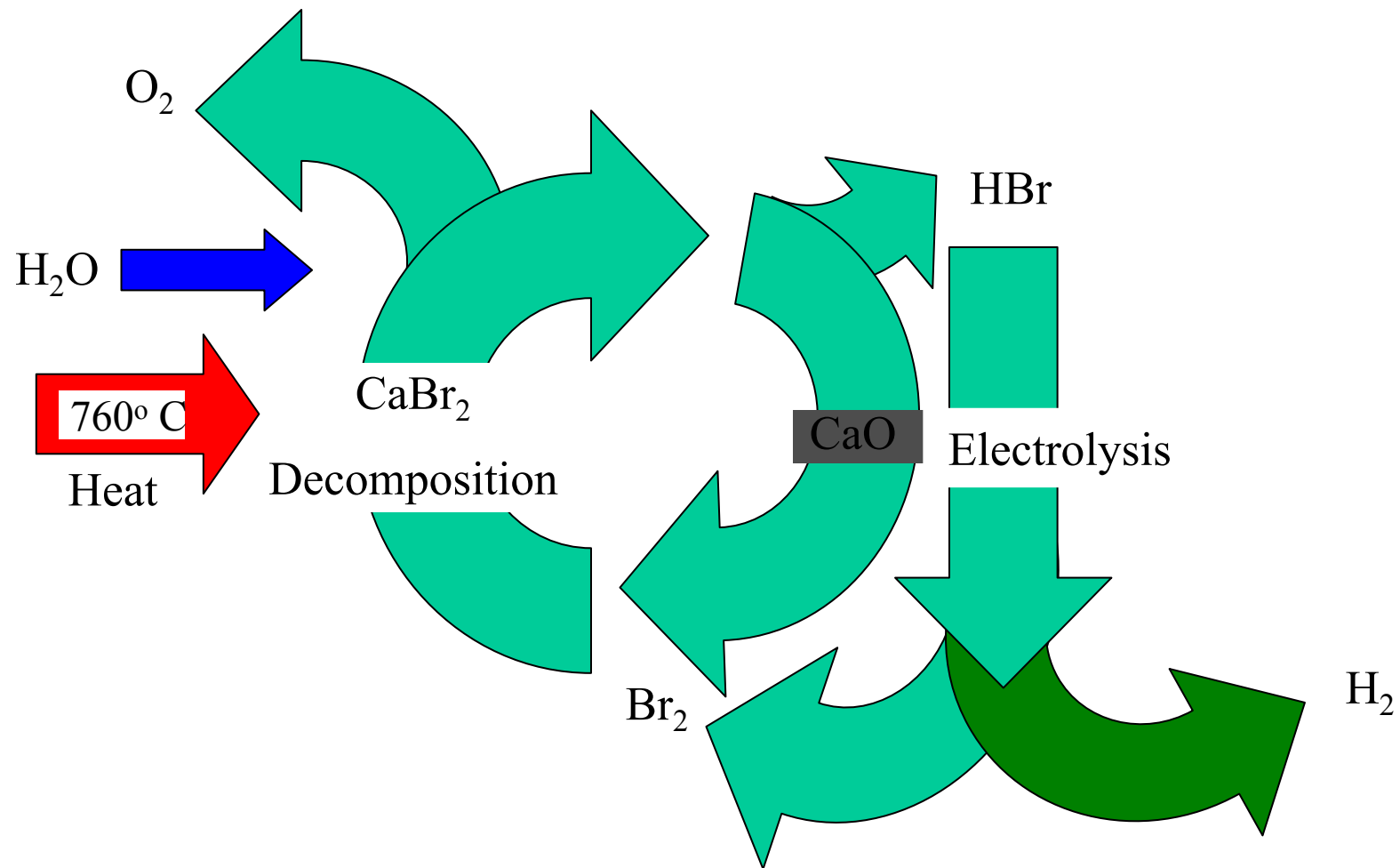
# Ca-Br-Fe Cycle (UT-3)





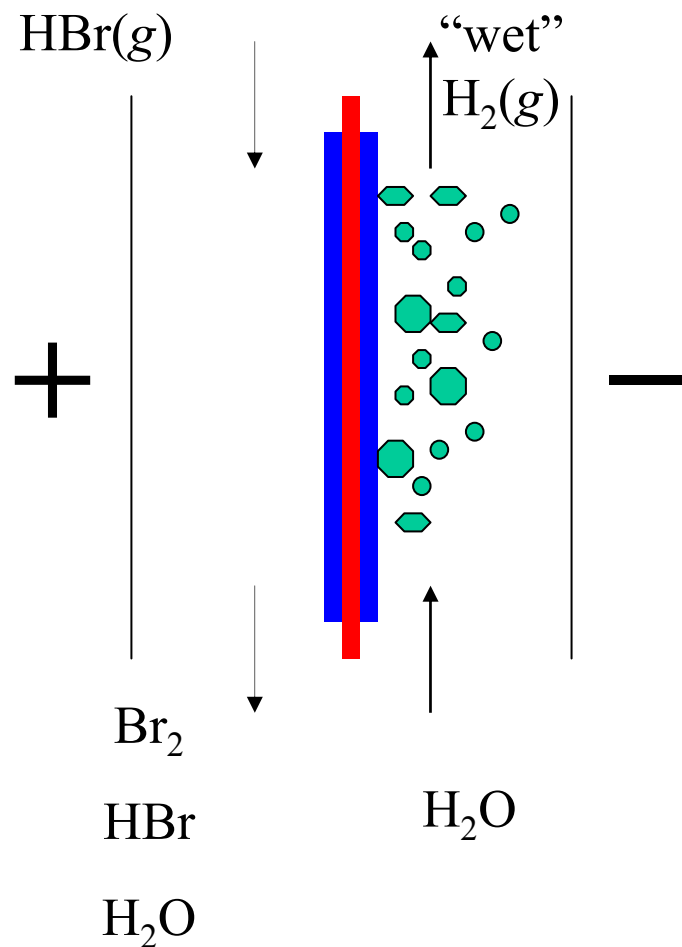


# Modified Ca-Br Cycle

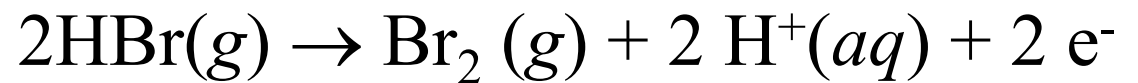




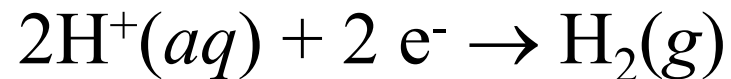
# Anhydrous HBr Electrolysis Using a PEM Reactor



Anode:



Cathode:



Overall:



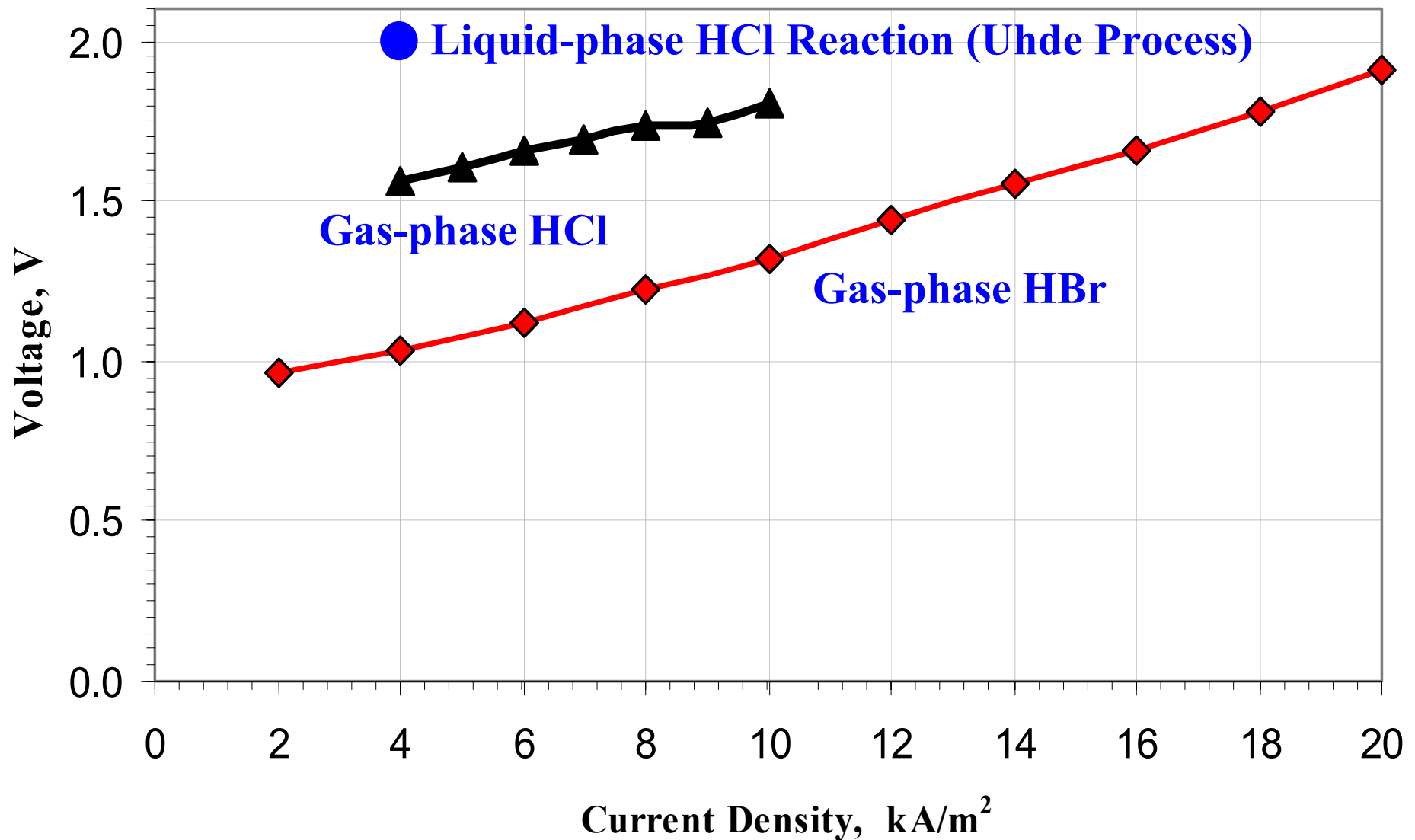
Anode Side Reaction:





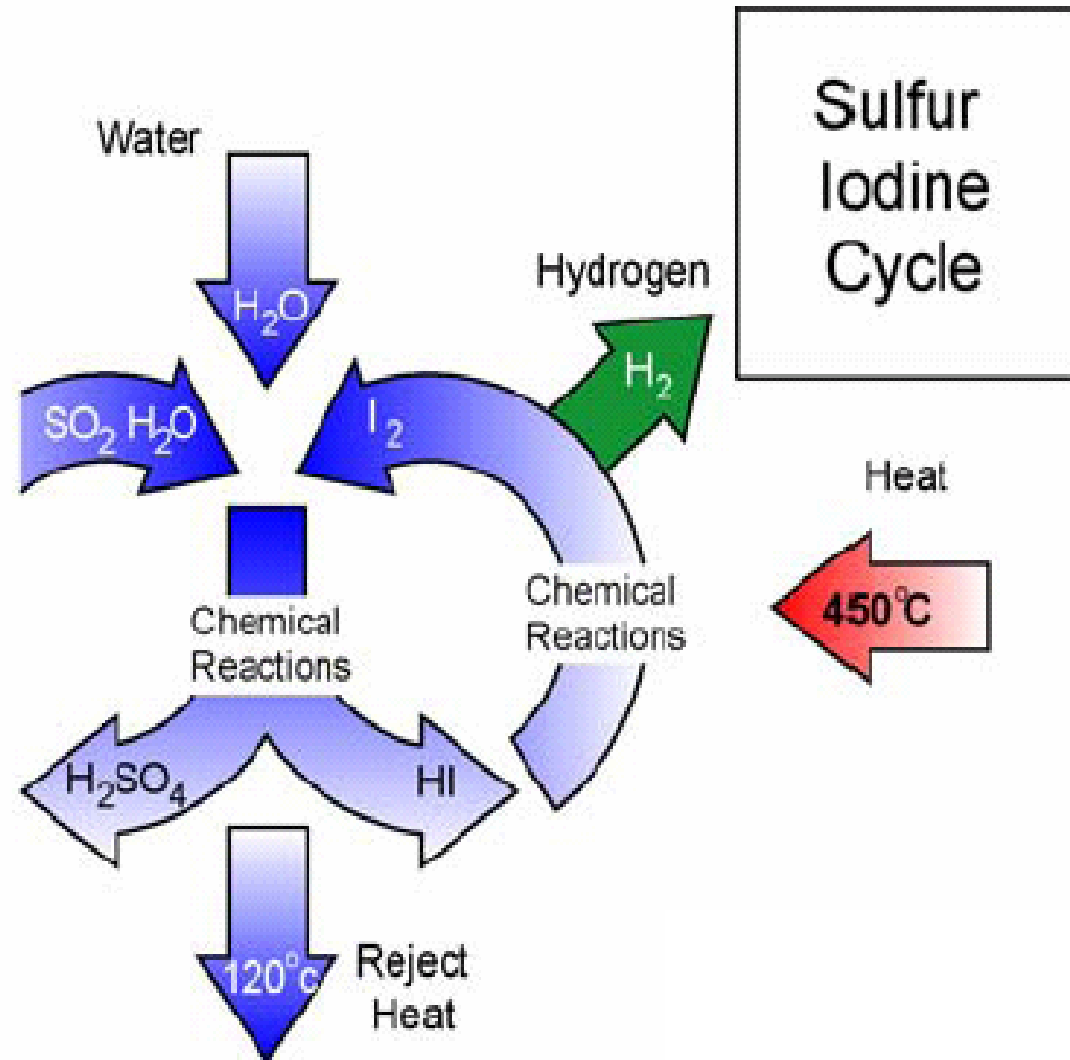
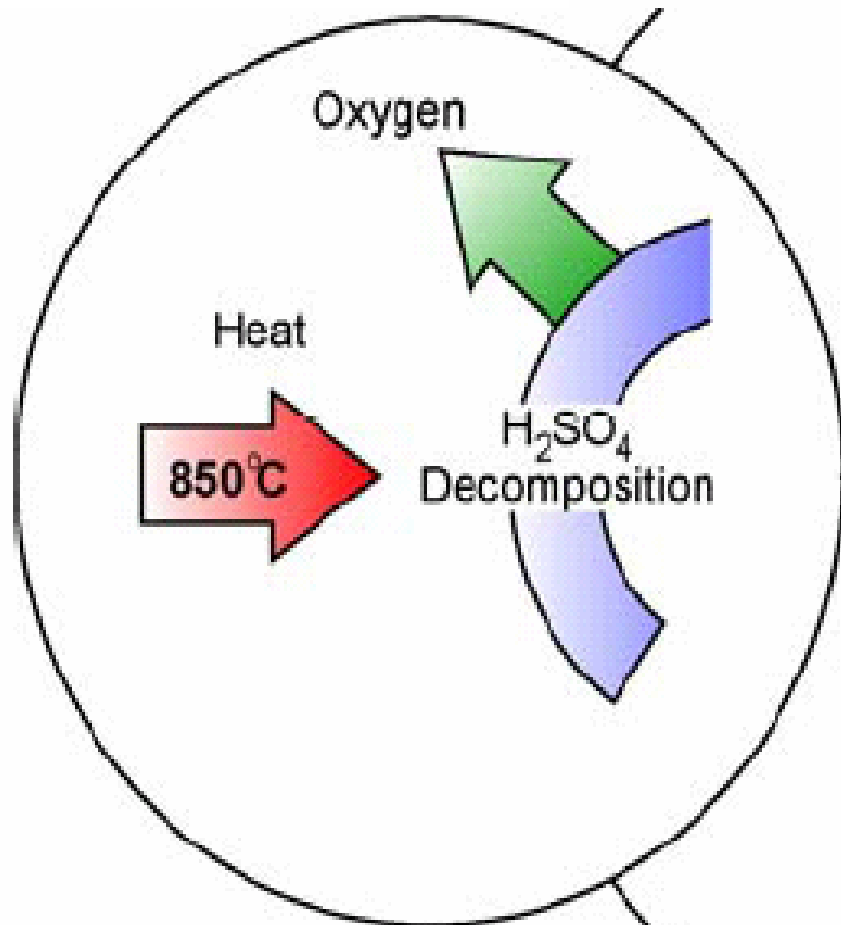
# Electrochemical Conversion of Halides

( $T=80^{\circ}\text{C}$ ;  $P=1.0\text{ atm}$ ;  $\text{RuO}_2$  catalyst)



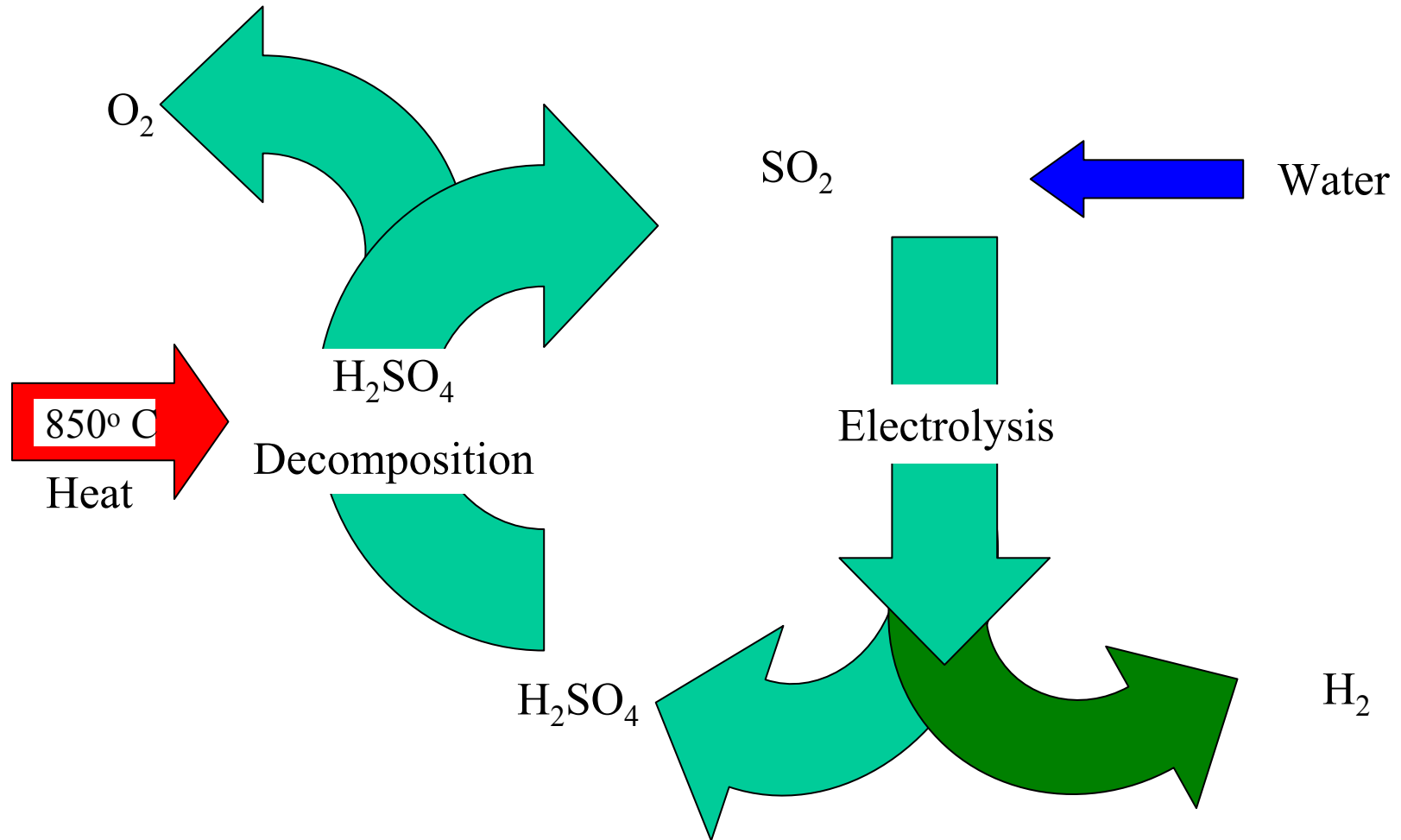


# Sulfur Iodine (S-I) Process



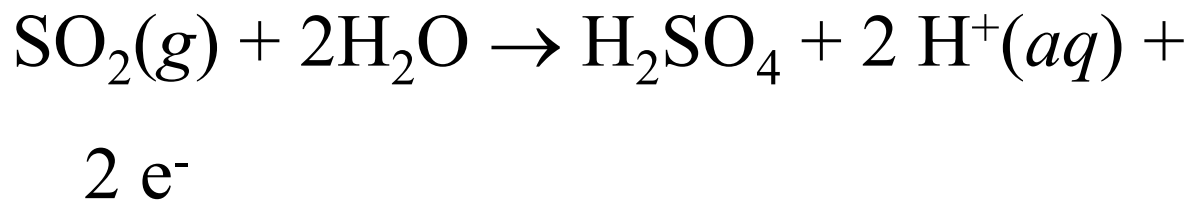


# Hybrid Sulfur (HyS) Process

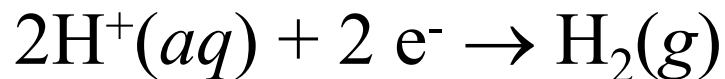


# Anhydrous SO<sub>2</sub> Electro-Oxidation Using a PEM Reactor

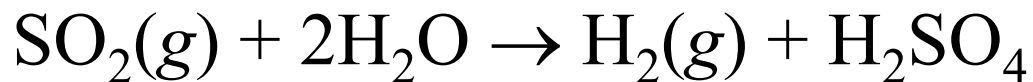
Anode:



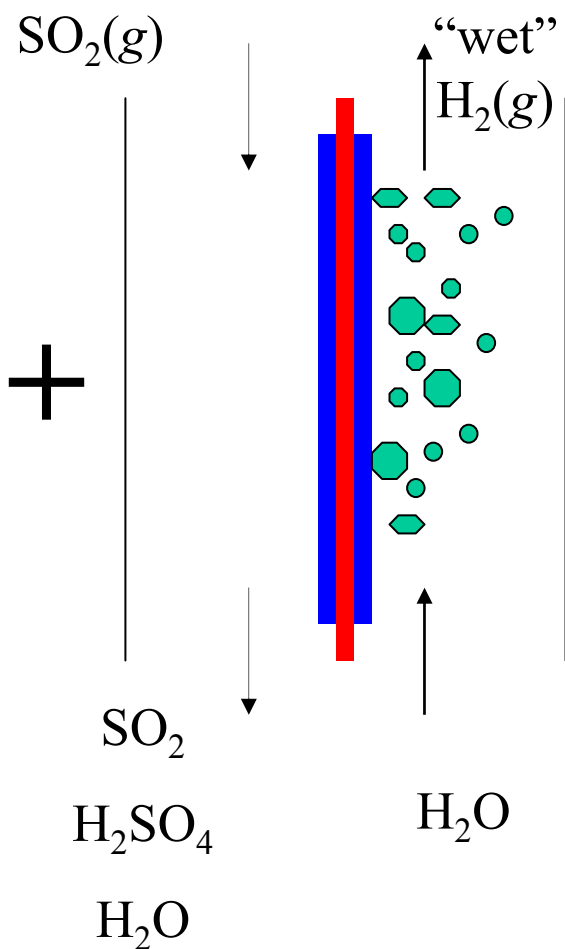
Cathode:



Overall:

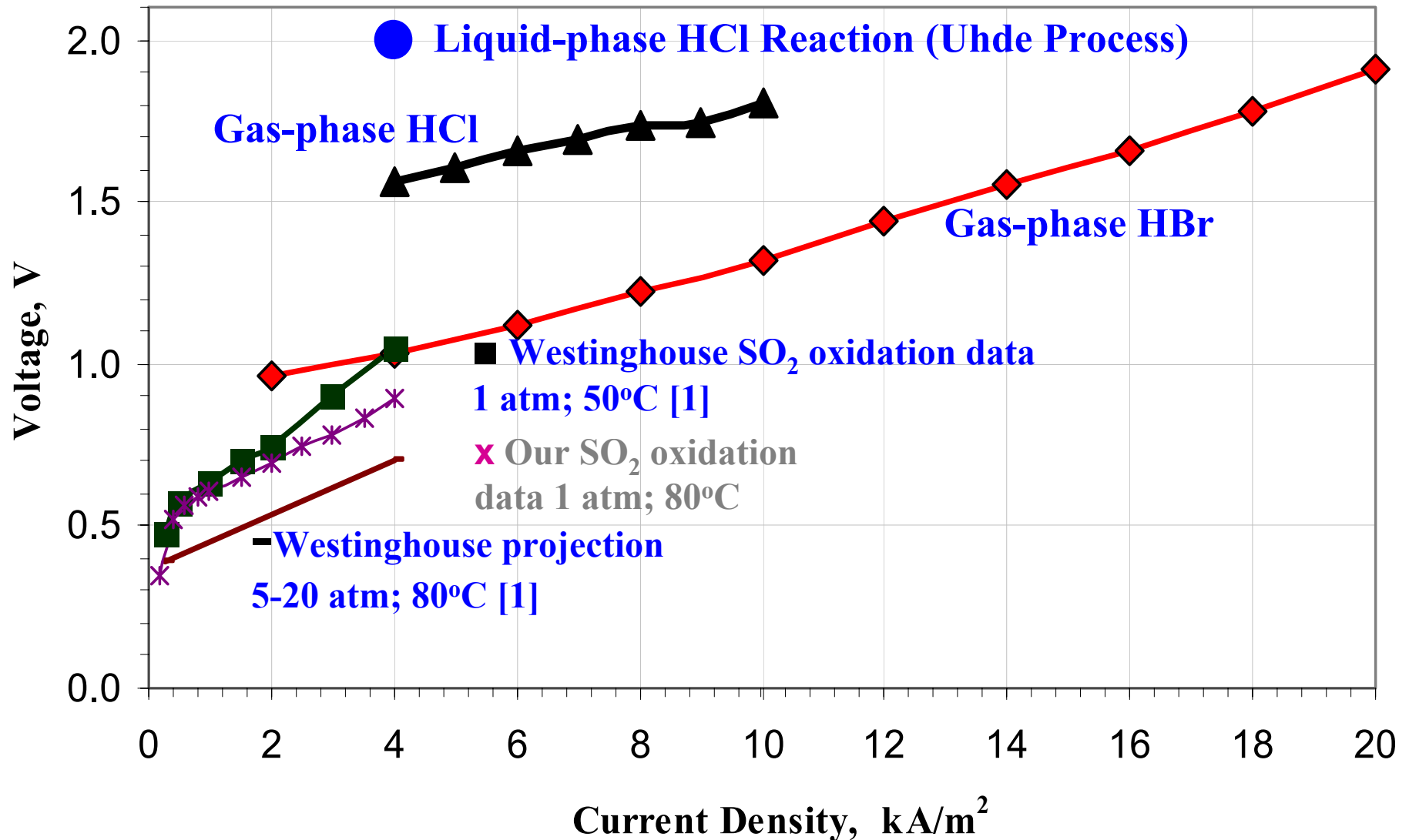


Poisoning Reaction:





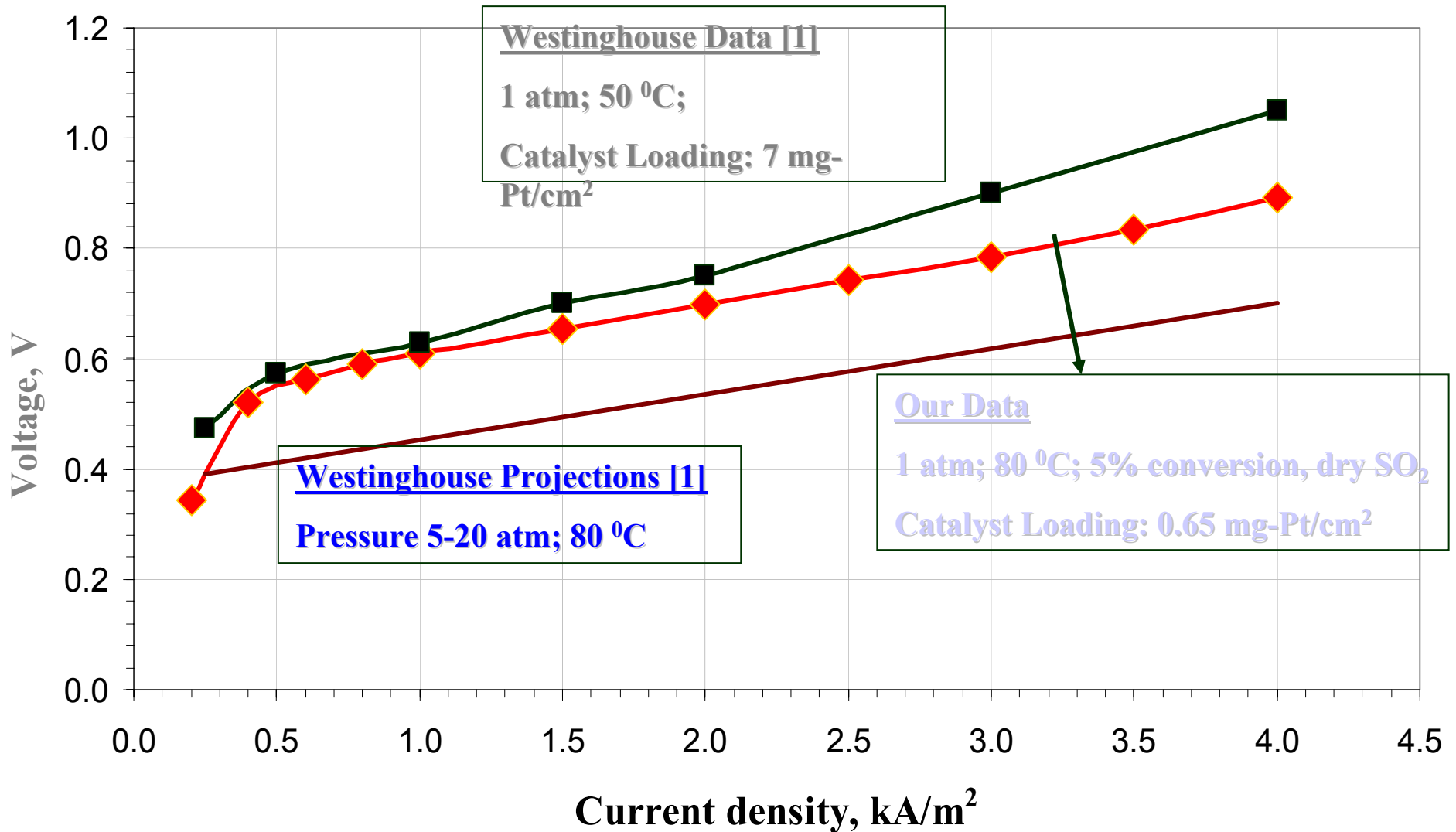
# Low Temperature Electrolysis



[1] P.W. Lu *et al.*, *J. Appl. Electrochem.*, 347 (1981).



# Oxidation of $\text{SO}_2$ to $\text{H}_2\text{SO}_4$

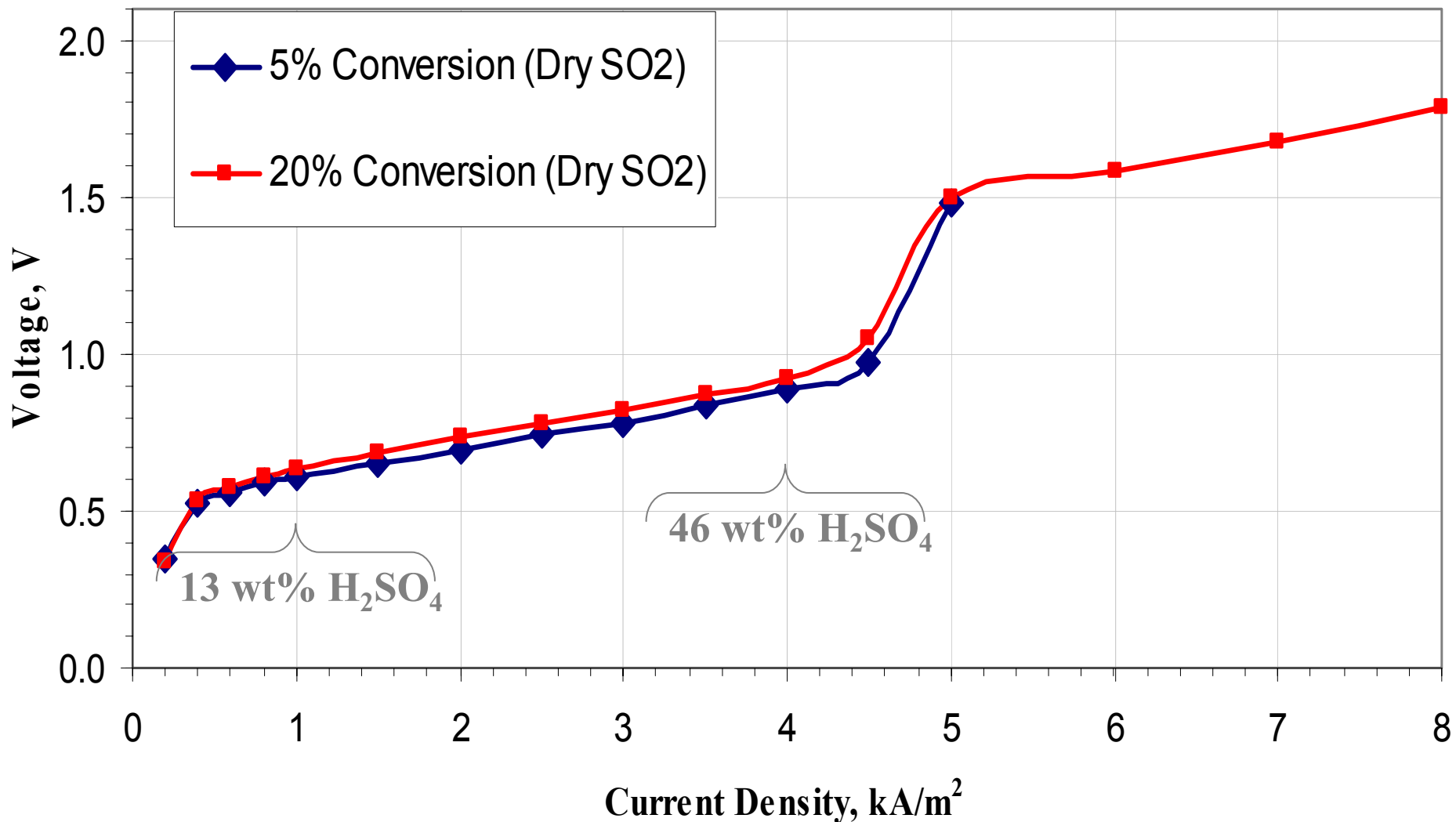






# Oxidation of $\text{SO}_2$ to $\text{H}_2\text{SO}_4$

( $T=80^\circ\text{C}$ ;  $P=1.0$  atm)





# Conclusions for Gas-Phase HBr Oxidation

- Electrochemical conversion of HBr to Br<sub>2</sub> and H<sub>2</sub> in a PEM reactor is very promising . (20 kA/m<sup>2</sup> @ < 2.0V)

## Future Work

- Measure performance as a function of temperature and pressure
- Develop mathematical models that can predict cell performance. These models could be fed into process flowsheet models being developed by Argonne National Laboratory.



# Conclusions for Gas-Phase SO<sub>2</sub> Oxidation

- Electrochemical conversion of SO<sub>2</sub> to H<sub>2</sub>SO<sub>4</sub> and H<sub>2</sub> in a PEM reactor is encouraging (*e.g.*, 4 kA/m<sup>2</sup> @ 0.9V).

## Future Work

- Measure performance as a function of temperature and pressure
- Develop mathematical models that can predict cell performance. Feed these models into process flowsheet models being developed by Savannah River National Laboratory.



# Technical Presentations

(speaker underlined)

- J. W. Weidner, P. Sivasubramanian, R. Ramasamy, C.E. Holland and F. Freire, “Electrochemical Generation of Hydrogen via Thermochemical Cycles,” The American Institute of Chemical Engineerings, Atlanta, GA, April, 2005.
- J. W. Weidner, P. Sivasubramanian, and F. Freire, “Electrochemical Conversion of Anhydrous HBr to Br<sub>2</sub> for Hydrogen Production,” The Electrochemical Society, Honolulu, HI, October, 2004. Please list any publications and presentations that have resulted from work on this project.



# Hydrogen Safety

We produce hydrogen via our electrochemical reactor. However, the concentrations are low and the vented in a hood. The risk of a hydrogen explosion or very low.